



DCP Midstream
3201 Quail Springs Parkway, Suite 100
Oklahoma City, OK 73134
405.605-3835 - Office
405.605-3896 - Fax

June 2, 2026

Chief Engineer
Air Quality Division
Oklahoma Department of Environmental Quality
P.O. Box 1677
Oklahoma City, OK 73101-1677

**RE: Individual Minor Source Operating Permit Application for an Oil and Gas Facility
DCP Operating Company, LP
Slapout Booster Station
Beaver County, Oklahoma**

Dear Sir/Madam:

DCP Operating Company, LP (DCP) owns and operates the Slapout Booster Station (Facility) located in Beaver County, Oklahoma. The Facility currently operates under the General Permit for Oil and Gas Facilities (GP-OGF) Operating Permit No. 2021-0124-O, issued on February 17, 2023, and converted to a Class II Authorization (2021-0124-O (M-1)) on August 12, 2024. The updated emissions calculations include three (3) 667-hp Superior 8G825 compressor engines, one (1) 300-bbl condensate storage tank, one (1) 210-bbl methanol storage tank, two (2) 25-bbl methanol tanks, condensate truck loading, blowdown emissions, maintenance, startup and shutdown emissions, and process piping fugitive emissions.

DCP is submitting an individual minor source operating permit application for the Facility and requests that Permit No. 2021-0124-O (M-1) be canceled upon the issuance of the individual operating permit. No new emission sources are being added with this application from those currently authorized by the GP-OGF, which includes Permit No. 2021-0124-O (M-1) and Notices of Modifications that have been submitted for engine changes. Emission estimates for maintenance, startups and shutdown (MSS) activities are represented, which were not required for prior permit applications. Emission estimates have been updated for the compressor blowdowns and fugitives based on a new site-specific gas sample.

Once the application is approved and the permit has been issued, please email the final permit to Jay Laughlin at jay.laughlin@p66.com and Stephen Ondak at stephen.r.ondak@p66.com. Your help is greatly appreciated and will assist us in aligning with the latest permitting procedures.

Introduction

This Application has been prepared in accordance with the requirements set forth in the OAC 252:100-7 and is considered to be a Tier I application with a web-based public notice requirement. This Application includes estimates of emissions from the emission sources at the Facility and the required ODEQ Permit Application forms for a minor source compressor station (DEQ Form 100-100) including the Oil and Gas Representative Sample Information Forms for oil and gas samples (refer to Attachment 10).

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Regulatory Applicability

The Facility, which falls under the North American Industrial Classification System (NAICS) code 211130 (formerly code 211111), provides compression of natural gas. The Facility is subject to Title 40 Code of Federal Regulations (CFR) Part 63 National Emission Standards for Hazardous Air Pollutants (NESHAP) MACT Subpart ZZZZ. The Facility is not subject to Part 61 NESHAP, Prevention of Significant Deterioration (PSD) permitting, or Title V Operating permits required under OAC 252:100-8.

NSPS Subpart Kb regulates volatile organic liquid storage vessels which were constructed, reconstructed or modified after July 23, 1984, and on or before October 4, 2023, with capacities greater than or equal to 75 cubic meters (471 barrels). NSPS Subpart Kc regulates volatile organic liquid storage vessels which were constructed, reconstructed or modified after October 4, 2023, with capacities greater than or equal to 75 cubic meters (471 barrels). There are four (4) storage vessels at the facility. One (1) storage tank (TNK-7) has a capacity of 300 barrels, one (1) tank (TNK-8) has the capacity of 210 barrels, and two (2) tanks (TNK-2; TNK-3) have a capacity of 25 barrels; therefore, not subject to these Subparts.

NSPS Subpart JJJJ regulates stationary spark ignition (SI) internal combustion engines (ICE). This Subpart was published as final in the Federal Register on January 18, 2008. The effective date of the rule is March 18, 2008. This Subpart affects natural gas-fired engines constructed after June 12, 2006, which are manufactured after July 1, 2008, for engines with horsepower (hp) between 100 and 500 hp. The three (3) engines at the Facility commenced construction prior to June 12, 2006, and are not subject to this Subpart.

NSPS Subpart OOOOb was published as final in the Federal Register on March 8, 2024. NSPS Subpart OOOOb regulates equipment at oil and natural gas production, transmission and distribution facilities that commenced construction, reconstruction, or modification after December 6, 2022. This Subpart regulates single well heads, centrifugal and reciprocating compressors, single and continuous bleed natural gas driven process controllers and pneumatic pumps, located at tank batteries, onshore natural gas processing plants and sweetening units. NSPS Subpart OOOO similarly regulates sources constructed, reconstructed or modified after August 23, 2011, and on or before September 18, 2015. NSPS Subpart OOOOa regulates sources constructed, reconstructed or modified after September 18, 2015, and on or before December 6, 2022. Four (4) storage tanks (TNK-7; TNK-8; TNK-2; TNK-3) and other potentially affected sources at the Facility were constructed prior to the effective dates of these Subparts and they are not subject. The engine changes have been like-kind replacements with no increase in capacity at the Facility.

MACT standards for reciprocating internal combustion engines (RICE MACT), 40 CFR Part 63 Subpart ZZZZ, were promulgated June 15, 2004. These standards apply to major sources of HAP emissions and regulate emissions from RICE with a site rating greater than 500 brake horsepower (Hp). The Facility is not classified as a major source of HAP emissions; however, it is an area source of HAPs and operates three (3) RICE engines with a site rating greater than 500 brake horsepower; therefore, RICE MACT requirements of Subpart ZZZZ are applicable.

Changes to Subpart ZZZZ which affect area sources of HAP were proposed on June 12, 2006. This subpart was published in the Federal Register as final on January 18, 2008. The effective date of the rule was March 18, 2008. This subpart affects new and reconstructed stationary RICE

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(after June 12, 2006) that are located at an area source of HAPs. Affected stationary RICE must meet the requirements of this Subpart by meeting the requirements of NSPS Subpart JJJJ, for spark ignition engines or Subpart IIII, for compression ignition.

Changes to Subpart ZZZZ which affect existing engines were proposed on June 7, 2012. This Subpart was published in the Federal Register as final on January 30, 2013. The effective date of the rule is April 1, 2013. This subpart affects existing stationary RICE (prior to June 12, 2006) that are located at an area source of HAPs. Affected 4SRB and 4SLB stationary RICE with a maximum engine power greater than 500 Hp are subject to emission limitations unless they are located in a "Remote Area". Existing engines located in a "Remote Area" with a maximum engine power greater than 500 Hp are subject to management practices. All existing stationary RICE engines with a horsepower rating less than 500 Hp are also subject to management practices. Three (3) natural gas-fired compressor engines (ENG-1a; ENG-2a; ENG-3) were constructed prior to June 12, 2006, and are subject to the area source maintenance requirements of NESHAP ZZZZ.

DCP will operate the Facility in compliance with applicable federal and state air quality regulations.

Facility Description

The Facility is a compressor station, responsible for the compression of natural gas. The natural gas stream enters the Facility and is compressed by three (3) natural gas-fired compressor engines into a pipeline for transmission from the Facility. Condensate generated at the site is stored in one (1) condensate storage tank (TNK-7). Condensate is loaded out from the Facility by truck (LOAD-1).

Attachment 2 of this Application presents a process flow diagram for the Facility, which is based on the equipment and operations.

Potential Emissions Calculations

The primary pollutants from the Facility are nitrogen oxides (NO_x), carbon monoxide (CO), and volatile organic compounds (VOC). Potential facility-wide emissions from the Facility are included in Attachment 3. Safety factors were added to calculated emissions to allow for changes in gas and liquid compositions and for operational flexibility.

Potential emissions from the natural gas-fired compressor engines were estimated for the Facility. Specifically, the potential NO_x, CO, VOC, and formaldehyde (H₂CO) emissions were based on manufacturer's data and AP-42, assuming 8,760 hours of operation per year and a catalytic converter in operation. The calculations are summarized in Attachment 4.

Potential emissions from the one (1) condensate storage tank (TNK-7) were calculated using ProMax process simulation software and a site-specific liquid sample. The calculations are summarized in Attachment 5.

Potential VOC emissions from condensate loading into trucks (LOAD-1) were estimated using ProMax process simulation software and a maximum annual throughput of 150,000 gallons per year. The calculations are summarized in Attachment 6.

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Potential VOC emissions from compressor blowdowns (BD-1) were estimated using engineering calculations and a site-specific gas analysis. The calculations are summarized in Attachment 7.

Potential VOC emissions from other MSS activities (MSS-1) were calculated using TCEQ default parameters and assumptions. The calculations are summarized in Attachment 8.

Potential VOC emissions from process piping fugitives (FUG-1) were estimated based on EPA's natural gas processing factors for process piping fugitive emissions and a site-specific gas analysis data from the facility. The calculations and gas analysis data are provided in Attachment 9.

Supporting Documentation and Attachments

To facilitate the ODEQ's review of this Application, DCP has included the following information:

- Attachment 1 – ODEQ Minor Facility Individual Permit Application Forms
- Attachment 2 – Facility Process Flow Diagram
- Attachment 3 – Facility-Wide Potential Emissions Summary Table
- Attachment 4 – Engine Potential Emissions Calculations
- Attachment 5 – Storage Tank Potential Emissions Calculations
- Attachment 6 – Truck Loading Potential Emissions Calculations
- Attachment 7 – Blowdown Potential Emissions Calculations
- Attachment 8 – MSS Potential Emissions Calculations
- Attachment 9 – Process Piping Fugitives Potential Emissions Calculations
- Attachment 10 – Oil and Gas Representative Sample Information Forms

In accordance with OAC 252:100-7, a check in the amount of \$750 is included in Attachment 1 of this Application.

ATTACHMENT 1

ODEQ Minor Facility Individual Permit Application Forms

DEQ LANDOWNER NOTIFICATION AFFIDAVIT

Tier I, II, or III permit applicants must provide notice to the landowner(s). The basis for this requirement is Title 27A of the Oklahoma Statutes, Supplement 1996, § 2-14-103(9), as described in OAC 252:4-7-13 (b).

Please note that you MUST fill out and return this affidavit even if you don't have to give any landowner notice.

A	NOTICE TO THE LANDOWNER(S) IS NOT REQUIRED because: (check one)
	My application does not involve any land.
	My application involves only land owned by me (or applicant business).
X	I have a current lease given to accomplish the permitted purpose.
	I have a current easement given to accomplish the permitted purpose.

OR

B	NOTICE TO THE LANDOWNER(S) IS REQUIRED because the land is owned by someone other than myself or the applicant business AND I HAVE NOTIFIED the following (check one):	
	Landowner(s)	Lessor or Administrator or Executor of the land
METHOD OF DELIVERY (check one):		
	Actual notice, for which I have a signed and dated receipt	
	Service by Sheriff or private process server, for which I have an affidavit	
	Service by certified mail, restricted delivery, for which I have a signed return receipt	
	Legal publication, for which I have an affidavit of publication from the newspaper, because the landowners could not be located through due diligence	

LANDOWNER AFFIDAVIT CERTIFICATION			
I, as the applicant or an authorized representative of the applicant, hereby certify that I own the real property, have a current lease or easement which is given to accomplish the permitted purpose (per Option A above), or have provided legal notice to the landowner(s) (per Option B above) about the permit application for the facility described below.			
Company Name	DCP Operating Company, LP	Facility Name	Slapout Booster Station
Facility Address or Legal Description.	Lat: 36.57751, Long: -100.05611 Section 04, T01N, R28E Beaver County, Oklahoma		
Responsible Official (signature)		Date Signed	6/9/2026
Responsible Official (typed)	Jay Laughlin	Title	P.E. Environmental

If the landowner notice applies to your application (Option B above) you can send the following form to them as your notice:

NOTICE TO LANDOWNER OF FILING	
Dear Landowner: (Name) _____	
(Applicant Name) _____ has filed a permit application with the Oklahoma Department of Environmental Quality for (Facility Name) _____ facility.	
This application involves the land owned by you located at:	
Address or Legal Description: _____	
Signed: _____	Date: _____

**AIR QUALITY PERMIT APPLICATION
GENERAL FACILITY INFORMATION**APPLICATION NUMBER
(AQD Use Only)

1	COMPANY INFORMATION	Name	DCP Operating Company, LP							
Mailing Address		3201 Quail Springs Parkway, Suite 100			City	Oklahoma City	State	OK	Zip	73134

2	APPLICATION TYPE	Applicability Determination		Construction Permit		☒	Operating Permit			
GP Authorization To Construct		GP Authorization To Operate		GP Name:						
Renewal		Modification		Relocation		PBR		PBR Type:		
Permit Number(s) (If Applicable)		2021-0124-O (M-1)								
Est. Date of Construction/Modification Start:		Completed		Operational Start-up:		Completed				
Construction Permit Public Review Process:		Traditional				Enhanced				

3	IS CONFIDENTIAL INFORMATION INCLUDED?	YES		☒	NO	
By including confidential information, Applicant acknowledges that such information may be shared with the U.S. Environmental Protection Agency for purposes consistent with the Federal Clean Air Act, 42 U.S.C. §§ 4201 et. seq.						

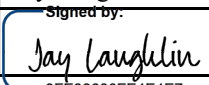
4	TIER CLASSIFICATION	☒	Tier I	☐	Tier II	☐	Tier III	☐	N/A – AD only
FACILITY TYPE		☐	Major	☒	Minor	☐	Synthetic Minor		

5	FEES SUBMITTED	\$750	Check #		Date	
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6	TECHNICAL CONTACT	Name	Jay Laughlin							
Phone		405.605.3835			Email Address		Jay.Laughlin@p66.com			
Company Name		DCP Operating Company, LP								
Street Address		3201 Quail Springs Parkway, Suite 100			City	Oklahoma City	State	OK	Zip	73134

7	FACILITY INFORMATION	Name	Slapout Booster Station								
SIC Code(s)		1311		NAICS Code(s)		211130					
Contact Person		Jay Laughlin			Title	Environmental		Phone	405.605.3835		
LEGAL DESCRIPTION		Sub Section	NW/4		Section	34		Township	03N	Range	18E
Physical Address or Driving Directions		From Slapout, OK, travel east on US-270/US 412 for 2.9 miles. Turn right onto N1650 Rd and go south for 2.7 miles to facility location on the east side of the road.									
City or Nearest Town		Slapout		Zip	73848		County	Beaver			

8	GEOGRAPHIC COORDINATES	Latitude (to 5 Decimals)		36.57751		Longitude (to 5 Decimals)		-100.05611		
REFERENCE POINT		☒	Facility Entrance Point or First Gate of Lease Property (preferred above all other options)							
Center of Facility		☐	Other (Specify):							

9	APPLICATION CERTIFICATION	This application, including all attachments, has been submitted as required by OAC 252:100. I certify that (a) I am the Responsible Official for this company as defined in OAC 252:100-1-3; and (b) based on information and belief formed after reasonable inquiry, the statements and information contained in this application are true, accurate, and complete.								
Responsible Official (name)		Jay Laughlin				Title	P.E. Environmental			
Responsible Official (signature)						Date	6/9/2026			
Phone		405.605.3835			Email Address		Jay.Laughlin@p66.com			
Street Address		3201 Quail Springs Parkway, Suite 100			City	Oklahoma City	State	OK	Zip	73134

EMISSION UNITS – SUMMARY

- For each affected facility under an NSPS or affected source under a MACT standard, provide the information requested in the table below
- For any control equipment listed here, provide supporting documentation of the control efficiency relied upon.
- For each engine, storage tank, and dehydration unit subject of this application, complete an equipment description table.
- Refer to Appendix F for De Minimis Activities that should be addressed in the application.

Emission Unit ID	Description (Make/Model, Capacity, Contents, Size, etc.)	Manufacture or Modification Date	Installed Date	Control Equipment (if any)		Subject to NSPS or NESHAP? If Yes, Specify Subpart	Appendix H Activity?		Subject to this Permit Action?
				Type	Capture / Control Efficiency (%)		Yes	No	
ENG-1a	Superior 8G825 667-hp	8/26/1970	2013	NSCR	NOx; CO - 70%	NESHAP MACT ZZZZ		X	Yes
ENG-2a	Superior 8G825 667-hp	1982	2021	NSCR	NOx; CO - 70%	NESHAP MACT ZZZZ		X	Yes
ENG-3	Superior 8G825 667-hp	7/1/1993; 2004	2013	NSCR	NOx; CO - 70%	NESHAP MACT ZZZZ		X	Yes
TNK-7	300-bbl Condensate Storage Tank	Pre-2011 (5/1989)	2013	None	None	--		X	Yes
TNK-8	210-bbl Methanol Storage Tank	Pre-2011 (2000)	2013	None	None	--		X	Yes
TNK-2	25-bbl Methanol Storage Tank	Pre-2011 (5/1989)	2013	None	None	--		X	Yes
TNK-3	25-bbl Methanol Storage Tank	Pre-2011 (7/1993)	2013	None	None	--		X	Yes
LOAD-1	Condensate Truck Loading	--	--	--	--	--		X	Yes
BD-1	Compressor Blowdown Emissions	--	--	--	--	--		X	Yes
MSS-1	Maintenance, Startups and Shutdowns	--	--	--	--	--		X	Yes
FUG-1	Process Piping Fugitive Emissions	--	--	--	--	--		X	Yes

EMISSION UNITS – ENGINES & TURBINES MINOR FACILITY

- Provide applicable information for each engine or turbine.
- For each engine or turbine, establish a NO_x, CO, VOC, and formaldehyde short-term (lb/hr) emission rate. Applicant may rely upon the CO surrogate policy to demonstrate compliance with formaldehyde limits. The lb/hr emission rates established will be incorporated into the permit, as necessary.
- Provide documentation of the emission factors used to determine lb/hr emissions, unless relying upon AP-42.
- Note any inherent limitations on HP, such as limits associated with the equipment coupled to an engine.

ENGINE DESIGN	Engine	☒	Turbine		Manufacture Date	Mfg 8/26/1970			
Emission Unit ID#	ENG-1a			Serial Number	20030				
Engine / Turbine Make	Superior			Model Number	8G825				
Fuel Type (NG, Diesel, etc.)	Field Gas	Equipped with Air Fuel Ratio Controller (AFRC)?			Yes	☒	No		
Type (check all that apply)	Lean-burn		Rich-burn	☒	4-stroke	☒	2-stroke		
Control Equipment	None		NSCR	☒	Oxidation Catalyst		Other: (specify)		
LB/HR CALCULATIONS	Maximum Rated HP			667	Btu/bhp-hr			8,000	
Pollutant	Factor (Units)			lb/hr	Source				
NO _x	3.0 (g/hp-hr)			4.41	Manufacturer Data AP-42				
CO	3.0 (g/hp-hr)			4.41	Manufacturer Data AP-42				
VOC	2.0 (g/hp-hr)			2.94	Manufacturer Data AP-42				
Formaldehyde	0.01 (g/hp-hr)			0.01	Manufacturer Data AP-42				
Comments:	Safety factor added to lb/hr calculations (10% for NO _x , CO, VOC and 200% for HCHO).								

ENGINE DESIGN	Engine	☒	Turbine		Manufacture Date	Mfg 1982			
Emission Unit ID#	ENG-2a			Serial Number	284369				
Engine / Turbine Make	Superior			Model Number	8G825				
Fuel Type (NG, Diesel, etc.)	Field Gas	Equipped with Air Fuel Ratio Controller (AFRC)?			Yes	☒	No		
Type (check all that apply)	Lean-burn		Rich-burn	☒	4-stroke	☒	2-stroke		
Control Equipment	None		NSCR	☒	Oxidation Catalyst		Other: (specify)		
LB/HR CALCULATIONS	Maximum Rated HP			667	Btu/bhp-hr			8,000	
Pollutant	Factor (Units)			lb/hr	Source				
NO _x	3.0 (g/hp-hr)			4.41	Manufacturer Data AP-42				
CO	3.0 (g/hp-hr)			4.41	Manufacturer Data AP-42				
VOC	2.0 (g/hp-hr)			2.94	Manufacturer Data AP-42				
Formaldehyde	0.01 (g/hp-hr)			0.01	Manufacturer Data AP-42				
Comments:	Safety factor added to lb/hr calculations (10% for NO _x , CO, VOC and 200% for HCHO).								

ENGINE DESIGN	Engine	X	Turbine		Manufacture Date	Mfg 7/1/1993		
Emission Unit ID#	ENG-3			Serial Number	301989			
Engine / Turbine Make	Superior				Model Number	8G825		
Fuel Type (NG, Diesel, etc.)	Field Gas	Equipped with Air Fuel Ratio Controller (AFRC)?			Yes	X	No	
Type (check all that apply)	Lean-burn		Rich-burn	X	4-stroke	X	2-stroke	
Control Equipment	None		NSCR	X	Oxidation Catalyst		Other: (specify)	
LB/HR CALCULATIONS	Maximum Rated HP			667	Btu/bhp-hr			8,000
Pollutant	Factor (Units)			lb/hr	Source			
NO _x	3.0 (g/hp-hr)			4.41	Manufacturer Data AP-42			
CO	3.0 (g/hp-hr)			4.41	Manufacturer Data AP-42			
VOC	2.0 (g/hp-hr)			2.94	Manufacturer Data AP-42			
Formaldehyde	0.01 (g/hp-hr)			0.01	Manufacturer Data AP-42			
Comments:	Safety factor added to lb/hr calculations (10% for NO _x , CO, VOC and 200% for HCHO).							

EMISSION UNITS - STORAGE TANKS MINOR FACILITY

- Tanks subject to this permit action identified in Form 100-100-A must submit supporting emission calculations or input and output files from emissions calculation software.
 - Working loss turnover (saturation) factor (K_N) should be set equal to 1 if the tanks are vapor balanced or have flashing emissions.
 - Flashing emissions from the produced water tanks may be calculated assuming 1% of the throughput is condensate or crude oil.
 - Capture efficiency is limited to 98%. Applicant may request a higher efficiency with additional monitoring and record keeping requirements to be established in the permit.
 - For floating roof storage tanks, please provide landing loss calculations.
 - Cleaning emissions are considered to be part of permitted tank emissions.
- Any new tank limits requested as part of this application are not in effect and may not be relied upon (e.g., for limiting applicability of 40 CFR Part 60, Subpart OOOOa requirements) until issuance of the corresponding permit. Please consult with a permit writer if you have questions or concerns after completing the enforceable limit eligibility review below.

Federally Enforceable Limits				
Eligibility Review				
Well Affected Facilities	Yes	☐	No	X
Are you requesting enforceable limits within 30 days after startup of production of the well(s)? If yes, please provide the startup date of well production 	Yes	☐	No	☐
Are you requesting enforceable limits for existing tanks with an initial PTE of less than 6 TPY as calculated based on the maximum average daily throughput as defined in §60.5430a.	Yes	☐	No	☐
Are you requesting enforceable limits for a new tank at an existing facility where the installation of the tank is unrelated to the modification of a well site? If yes, the enforceable limit must be requested prior to startup of the new tank.	Yes	☐	No	☐
Compressor Station or Gas Processing Plant	Yes	X	No	☐
Are you requesting enforceable limits prior to startup of the compressor station or onshore natural gas processing plant? If yes, please provide the startup date of the compressor station or onshore natural gas processing plant. 	Yes	☐	No	X
Are you requesting enforceable limits for a tank after the startup of the compressor station or onshore natural gas processing plant? If yes, the enforceable limit must be requested prior to startup of the new tank.	Yes	☐	No	X
VRU Removal	Yes	☐	No	X
Are you requesting enforceable limits for tanks within 30 days of removal of the VRU from operation? If yes, please provide the date of removal from operation. 	Yes	☐	No	☐
<i>If you answer no to the question applicable to your facility/situation, you may not be eligible for enforceable limits.</i>				
Enforceable Limits Request	Tank Number(s)		Requested Limit (TPY)	
The listed tanks and requested limits will be included in the permit. <b style="color: red;">Federally Enforceable Limits Not Requested	N/A		N/A	

Tanks Not Requesting Federally Enforceable Limits	
	Emission Unit ID #
List tanks not requesting enforceable limits	TNK-7
	TNK-8
	TNK-2
	TNK-3

Fixed Roof

Parameter (Tank IDs) ¹	TNK-7	TNK-8	TNK-2	TNK-3
Contents	Condensate	Methanol	Methanol	Methanol
Throughput, gal/yr	150,000	150,000	125,000	125,000
Working/Breathing Calculation Method/Tool	ProMax	ProMax	ProMax	ProMax
Working/Breathing Emissions, TPY	1.24	0.28	0.04	0.04
Flash Calculation Method/Tool	ProMax	ProMax	ProMax	ProMax
Flashing Emissions, TPY	2.13	0.00	0.00	0.00
Cleaning Calculation Method/Tool	--	--	--	--
Cleaning Emissions, TPY	--	--	--	--
Control Type, see Appendix D	None	None	None	None
Capture Efficiency, %	--	--	--	--
Control Efficiency, %	--	--	--	--
Tank VOC Emitted at Tank, TPY	--	--	--	--
Tank VOC Emitted at Flare, TPY	--	--	--	--
Total VOC Emissions, TPY	3.38	0.56 <i>(With 100% Added Safety Factor)</i>	0.08 <i>(With 100% Added Safety Factor)</i>	0.08 <i>(With 100% Added Safety Factor)</i>
Benzene, TPY	--	--	--	--
Toluene, TPY	--	--	--	--
Ethylbenzene, TPY	--	--	--	--
Xylene, TPY	--	--	--	--
n-Hexane, TPY	--	--	--	--
Total HAP, TPY	--	--	--	--

¹ Multiple tanks may be grouped by liquid.

LOADING EMISSIONS

MINOR FACILITY

- Emissions from loading condensate and produced water into tank trucks should be estimated using AP-42 (6/08), Section 5.2, Equation 1. Applicant should consult with AQD if proposing a different calculation method.
- Emissions routed to the tanks are distributed and represented at the tanks.
- Emissions from produced water loading may be calculated assuming 1% of the throughput is condensate or crude oil.

Liquids Loaded	Condensate	
Throughput, gal/yr	150,000	
Saturation Factor	0.6	
Temp., °F	57.93	
TVP, psia	3.54	
MW, lb/lb-mol	51.43	
VOC, wt.%	100	
Emission Factor, lb/10³ gal ⁽¹⁾	2.36	
Control Method Efficiency (see Appendix C)	--	
Capture Efficiency, %	--	
VOC Emitted at Truck, TPY	0.18	
VOC Routed to Control, TPY	--	
VOC Routed to Tanks, TPY ⁽²⁾	--	
Total VOC Emissions, TPY	1.50 <i>A 750% Safety Factor Added</i>	
Benzene, TPY	--	
Toluene, TPY	--	
Ethylbenzene, TPY	--	
Xylene, TPY	--	
n-Hexane, TPY	--	
Total HAP, TPY	--	

⁽¹⁾ Final factor considering any VOC reduction stated for methane/ethane.

⁽²⁾ For when emissions from loading are routed to a tank the emissions shall be included in determining compliance with the tank emission limits.

FUGITIVE EMISSIONS

MINOR FACILITY

- Fugitive VOC emissions need to be included in the emissions calculations to determine major source status for any facility with a storage tank subject to, or grandfathered from, NSPS Subpart K or Ka.
- Separate tables may be necessary for controlled and uncontrolled sources or affected and unaffected sources under NSPS Subparts KKK, OOOO, OOOOa.
- The emission factors shown are the Oil and Gas Production Operations factors from the “Protocol for Equipment Leak Emission Estimates” EPA-453/R-95-017. Other factors may be used, if applicable.
- Any form or spreadsheet containing the same relevant information may be substituted for this form.

FUGITIVE EMISSION SOURCES			Emission Unit ID#		FUG-1		
Source Type	Service ¹	Number of Sources	Emissions Factor, lb/hr/source	Weight % VOC	VOC Emissions		Type of Control
					lb/hr	TPY	
Valves	Gas	383	0.00992	23.20	0.88	3.86	None
	Light Oil	38	0.0055	100	0.21	0.92	None
	Heavy Oil	--	--	--	--	--	--
	Water/Oil	--	--	--	--	--	--
Pump Seals	Gas	--	--	--	--	--	--
	Light Oil	--	--	--	--	--	--
	Heavy Oil ³	--	--	--	--	--	--
	Water/Oil	--	--	--	--	--	--
Connectors	Gas	1015	0.00086	23.20	0.20	0.89	None
	Light Oil	3	0.0002	100	0.00	0.00	None
	Heavy Oil	--	--	--	--	--	--
	Water/Oil	--	--	--	--	--	--
Flanges	Gas	34	0.00086	23.20	0.01	0.03	None
	Light Oil	--	--	--	--	--	--
	Heavy Oil	--	--	--	--	--	--
	Water/Oil	--	--	--	--	--	--
Open-ended lines	Gas	--	--	--	--	--	--
	Light Oil	--	--	--	--	--	--
	Heavy Oil	--	--	--	--	--	--
	Water/Oil	--	--	--	--	--	--
Other ² (Compressor Seals; Relief Valves)	Gas	25	0.0194	23.20	0.11	0.49	None
	Light Oil	--	--	--	--	--	--
	Heavy Oil	--	--	--	--	--	--
	Water/Oil	--	--	--	--	--	--
					TOTAL	7.74	<i>With 25% Added Safety Factor</i>

Notes: 1. Heavy oil has an API gravity of less than 20°. Water/oil is any water stream in oil service with water content greater than 50% up to water content of 99%.

2. The “Other” equipment type includes **compressors**, pressure relief valves, **relief valves**, diaphragms, drains, dump arms, hatches, instruments, meters, polished rods, and vents. This “Other” equipment type should be applied for any equipment type other than connectors, flanges, open-ended lines, pumps, or valves.

3. No EF for pumps in heavy oil service was provided in the EPA document as no data was collected in the API study. This is a suggested factor from a June 2018, TCEQ memorandum without the estimated control efficiency for the TX LDAR program.

OTHER NSPS AFFECTED EQUIPMENT

MINOR FACILITY

Pneumatic Devices

Device Type	Number of Devices	Subject to NSPS (if not provide reason)
Continuous Bleed Natural Gas Driven Pneumatic Controller		
Natural Gas Driven Diaphragm Pumps		

Centrifugal Compressors Using Wet Seals

Manufacturer / Model	Serial Number or Unique Identifier	Compressor Rated HP	Manufacture Date	Subject to NSPS (if not provide reason)

Reciprocating Compressors

Manufacturer / Model	Serial Number or Unique Identifier	Compressor Rated HP	Manufacture Date	Subject to NSPS (if not provide reason)
Superior 8G825; Joy Compressor	ENG-1a (SN: 20030); Comp (SN: 57847)	ENG-1a: 667	ENG-1a: 8/26/1970 Comp: Pre-2011 (~1970s)	No; Manufacture Date
Superior 8G825; Joy Compressor	ENG-2a (SN: 284369); Comp (SN: 207375)	ENG-2a: 667	ENG-2a: 1982 Comp: Pre-2011 (~1970s)	No; Manufacture Date
Superior 8G825; Joy Compressor	ENG-3 (SN: 301989); Comp (SN: F12507)	ENG-3: 667	ENG-3: 7/1/1993 Comp: Pre-2011	No; Manufacture Date

MAINTENANCE, STARTUP, AND SHUTDOWN (MSS) MINOR FACILITY

- MSS emissions are part of normal operation of a source and should be accounted for in planning, design, and implementation of operating procedures for process and control equipment. As such, MSS emissions should be included in Potential to Emit (PTE) calculations and are subject to applicable permitting requirements.
- Facility shall estimate MSS emissions to the extent that they are predictable and quantifiable. Please identify and explain “other” MSS emissions listed.

Parameter	Emissions (TPY)
Blowdown \ Venting Emissions or Activities	
VOC	3.73 <i>(With 25% Added Safety Factor)</i>
Other MSS Activities, Identify Each Activity	See Attachment 8
NO _x	
CO	
VOC	1.01 <i>(With 250% Added Safety Factor)</i>
PM _{2.5}	<0.01
PM ₁₀	0.001
SO ₂	
Other Pollutant	
Total Emissions	4.74
VOC	
NO _x	
CO	
PM _{2.5}	
PM ₁₀	
SO ₂	
Other Pollutant	
Benzene	
Toluene	
Ethylbenzene	
Xylene	
n-Hexane	
Total HAP	0.0002

SUPPORTING DOCUMENTS AND EMISSION CALCULATIONS

MINOR FACILITY

- Please use this checklist to identify supporting documentation submitted for emission units and emissions calculations subject to this permitting action including any changes to existing equipment or emission.
- When relying on process emissions calculation software or process simulator the input (parameters and composition) and output or stream reports must be included.

Supporting Documents and Emission Calculations Attached	Yes	No
Amine Unit emission calculations		X
Glycol Dehydration Unit emission calculations		X
Tank emission calculations and include the following:	X	
Flashing emissions	X	
Working and breathing emissions	X	
Landing emissions		X
Cleaning emissions		X
Loading emissions calculations	X	
Fugitive emission calculations	X	
MSS emission calculations	X	
Appendix H Activities emission calculations (not otherwise addressed)		X
Process flow diagrams	X	
Representative Sample Guidance Forms DEQ 100-702 and required sample reports	X	
40 CFR Part 63 Subpart HH Facility Registration Form DEQ 100-401		X
EPA Engine Certification		X
Manufacturer Emission Data Sheet(s) for all engines and engine control equipment	X	
H ₂ S content analysis of inlet gas stream for Amine Units		X
Site specific dispersion modeling if the facility cannot meet the criteria identified in Appendix E		X
Please indicate if this application is being used as notification under any applicable NSPS and NESHAP and attach information as required by the individual federal rule and general requirements under 40 CFR §60.7 (a).		X

AIR QUALITY DIVISION CLASSIFICATION OF AQ PERMIT APPLICATIONS & APPLICATION FEES		Application Number (AQD Use Only)	

Company Name	DCP Operating Company, LP						
Facility Name	Slapout Booster Station						
Mailing Address	3201 Quail Springs Parkway, Suite 100	City	Oklahoma City	State	OK	Zip	73134

This form is used to document both a preliminary determination of the Tier classification and any associated Application Fee.

Step 1: APPLICATION CLASSIFICATION AND TIER DETERMINATION

DEQ's "Uniform Permitting" system, under OAC 252:004, categorizes different types of applications as Tier I, II, or III, depending on their complexity and the amount of public interest. The main effect of a Tier classification is the amount of public review given the application. For Air Quality permits, Tier I basically includes minor facilities and most synthetic minor facilities. Tier II covers major sources, and Tier III covers only very large sources such as those requiring PSD review. Additional information to make a preliminary determination of the Tier classification is provided on the next page. This determination will be verified before permit issuance.

Note that all Tier II and III applications require public notice of the application in one newspaper local to the site or facility as soon after the filing date as possible. Other public participation requirements, such as notice of draft and proposed permit, and notice of public meeting may also be required. Contact our office for more information on these requirements.

TIER CLASSIFICATION	X	Tier I		Tier II		Tier III		N/A – AD only
FACILITY TYPE		Major		Minor	X	Synthetic Minor	Confirmed/Corrected by: (AQD Use Only)	

Step 2: APPLICATION TYPE & FEE

Application fee may be determined according to the following schedule. The emissions level is based on the single criteria pollutant with the highest emissions rate. Fees are subject to change – please refer to OAC 252:100-7-3 or 252:100-8-1.7 for the latest fee schedule.

MAJOR SOURCE		Fee	MINOR OR SYNTHETIC MINOR FACILITY		Fee
	Applicability Determination (100734)	\$500		Applicability Determination (100922)	\$500
	GP- Authorization to Construct (100778)	\$900		PBR – Construct (100985)	\$250
	GP- Authorization to Operate (100788)	\$900		PBR – Operate (100989)	\$100
	Part 70 Construction (100150)	\$7,500		GP – Authorization to Construct (100826)	\$500
	Part 70 Construction Modification (100779)	\$5,000		GP – Authorization to Operate (100827)	\$500
	Part 70 Operation (100733)	\$7,500		Construction (100829)	\$2,000
	Part 70 Minor Modification (100781)	\$3,000		Permit Amendment – no emission increase (100830)	\$500
	Part 70 Significant Modification (100786)	\$6,000	X	Operating Permit (100831)	\$750
	Part 70 Renewal (100787)	\$7,500		Operating Permit Modification (100833)	\$750
	Part 70 Relocation (100782)	\$500		Relocation (100834)	\$250

Application Type Confirmed – (AQD Use Only)

GP or PBR Name (If Applicable):		Existing Permit Number (If Applicable)	2021-0124-O (M-1)
------------------------------------	--	---	-------------------

PAYMENT INFORMATION

Please choose one payment type and attach payment – payable to the Department of Environmental Quality (no cash can be accepted). Please reference the facility name (or existing permit or Authorization number) on the check or money order.

Payment Type	Check	Money order	Amount/ Receipt Confirmed by: (DEQ Use Only)	
Amount:	\$750	Check or Money Order Number:		Date:

TIER DETERMINATION INFORMATION

OAC 252:004-7 categorizes different types of Air Quality applications as Tier I, II, or III, depending on their complexity and the amount of public interest under DEQ's "Uniform Permitting" system. The Tier classification affects the amount of public review given the application. Applicants may use the following as a checklist for determining Tier classification.

OAC 252:4-7-32. Air quality applications - Tier I**No Public Notice Requirement**

- ☐ (1) Relocation permit for a minor facility.
- ☐ (2) Modification of an existing FESOP that is based on the operating conditions of a construction permit that was processed under Tier I and completed the web-based public notice requirement and does not differ from those construction permit conditions in any way considered significant. [FESOP Enhanced NSR]
- ☐ (3) Extension of expiration date of a minor facility construction permit.
- ☐ (4) Modification of any Part 70 source operating permit condition that is based on the operating conditions of a construction permit that was processed under Tier I (with web-based public notice), Tier II, or Tier III and OAC 252:100-8-8 and does not differ from those construction permit conditions in any way considered significant under OAC 252:100-8-7.2(b)(2). [Enhanced NSR]
- ☐ (5) Extension of expiration date of a Part 70 source's construction permit.
- ☐ (6) New, modified, and renewed individual authorizations under general permits for which a schedule of compliance is not required by OAC 252:100-8-5(e)(8)(B)(i).
- ☐ (7) Burn approvals.
- ☐ (8) Administrative amendments of all air quality permits and other authorizations.

No Public Notice Requirement, 45-Day EPA Review Requirement

- ☐ (1) Minor modification to a Part 70 source operating permit where the facility obtained a prior construction permit for the modification as required by OAC 252:100-8-4(a)(1)(B)(iv). [Traditional NSR]
- ☐ (2) Minor modification under OAC 252:100-8-7.2(b)(1) to a Part 70 source operating permit that did not trigger an NSR permitting action.

Web-based Public Notice Requirement

- ☐ (1) New minor NSR construction permit for a minor facility.
- ☒ (2) Initial operating permit for a new minor facility.
- ☐ (3) Modification of a construction permit for a minor facility.
- ☐ (4) Modification of an existing minor operating permit that was issued prior to September 15, 2021, and that will now become a FESOP.
- ☐ (5) Modification of a minor operating permit that did not undergo the *FESOP Enhanced NSR Process*. [Traditional NSR]
- ☐ (6) Construction permit for an existing Part 70 source as required by OAC 252:100-8-4(a)(1)(B)(iv).

OAC 252:4-7-33. Air quality applications - Tier II

- ☐ (1) A minor facility seeking a permit for a facility modification that when completed would turn it into a Part 70 source.
- ☐ (2) Any permit application for a Part 70 source that would result, on issuance, with the facility being covered by a FESOP (PBR, GP, or individual facility operating permit).
- ☐ (3) Construction permit for a new Part 70 source not classified under Tier III.
- ☐ (4) Construction permit for an existing Part 70 source for any facility change considered significant under OAC 252:100-8-7.2(b)(2) and which is not classified under Tier III.
- ☐ (5) Initial operating permit for a Part 70 source.
- ☐ (6) Acid rain permit that is independent of a Part 70 permit application.
- ☐ (7) Temporary source permit under OAC 252:100-8-6.2.
- ☐ (8) Significant modification, as described in OAC 252:100-8-7.2(b)(2), of a Part 70 operating permit or a modification of a Part 70 operating permit incorporating a Tier II construction permit that did not undergo the *Enhanced NSR Process*.
- ☐ (9) Modification of a Part 70 operating permit when the conditions proposed for modification differ from the underlying construction permit's operating conditions in any way considered significant under OAC 252:100-8-7.2(b)(2).
- ☐ (10) A construction permit modification considered significant under OAC 252:100-8-7.2(b)(2) and which is not classified under Tier III.
- ☐ (11) Renewals of operating permits for Part 70 sources.
- ☐ (12) New, modified, and renewed general permits.
- ☐ (13) Individual authorizations under any general permit for which a schedule of compliance is required by OAC 252:100-8-5(e)(8)(B)(i).
- ☐ (14) Plant-wide emission plan approval under OAC 252:100-37-25(b) or OAC 252:100-39-46(j).

OAC 252:4-7-34. Air quality applications - Tier III

- (a) A construction permit for any new major stationary source listed in this subsection requires a Tier III application. For purposes of this section, "Major stationary source" means:

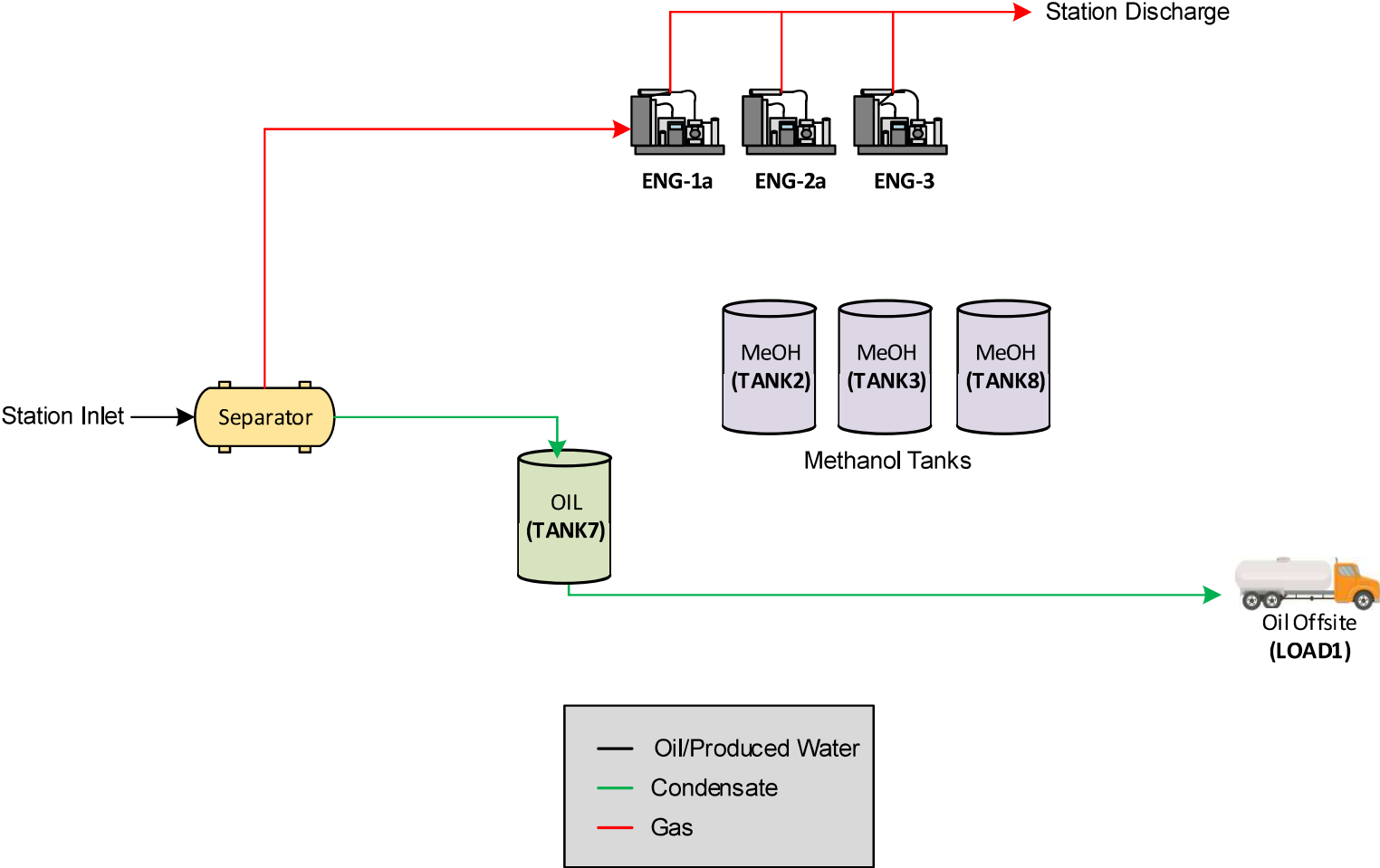
- | | |
|--|--|
| ☐ (1) Any of the following sources of air pollutants which emits, or has the PTE, 100 TPY or more of any pollutant subject to regulation: | |
| ☐ (A) carbon black plants (furnace process), | ☐ (N) incinerators, except where used exclusively as air pollution control devices, |
| ☐ (B) charcoal production plants, | ☐ (O) petroleum refineries, |
| ☐ (C) chemical process plants, | ☐ (P) petroleum storage and transfer units with a total storage capacity exceeding 300,000 barrels, |
| ☐ (D) coal cleaning plants (with thermal dryers), | ☐ (Q) phosphate rock processing plant, |
| ☐ (E) coke oven batteries, | ☐ (R) Portland cement plants, |
| ☐ (F) fossil-fuel boilers (or combustion thereof), totaling more than 250 million BTU per hour heat input, | ☐ (S) primary aluminum ore reduction plants, |
| ☐ (G) fossil fuel-fired steam electric plants of more than 250 million BTU per hour heat input, | ☐ (T) primary copper smelters, |
| ☐ (H) fuel conversion plants, | ☐ (U) primary lead smelters, |
| ☐ (I) glass fiber processing plants, | ☐ (V) primary zinc smelters, |
| ☐ (J) hydrofluoric, sulfuric or nitric acid plants, | ☐ (W) secondary metal production plants, |
| ☐ (K) iron and steel mill plants, | ☐ (X) sintering plants, |
| ☐ (L) Kraft pulp mills, | ☐ (Y) sulfur recovery plants, or |
| ☐ (M) lime plants, | ☐ (Z) taconite ore processing plants, and |

- ☐ (2) Any other source not specified in paragraph (1) of this definition which emits, or has the PTE, 250 TPY or more of any pollutant subject to regulation.
- (b) Existing incinerators. An application for any change in emissions or potential to emit, or any change in any permit condition, that would have caused an incinerator to be defined as a major stationary source when originally permitted shall require a Tier III application.

ATTACHMENT 2

Facility Process Flow Diagram

PROCESS FLOW DIAGRAM
SLAPOUT BOOSTER STATION
DCP OPERATING COMPANY, LP



ATTACHMENT 3

Facility-Wide Potential Emissions Summary Table

FACILITY-WIDE POTENTIAL EMISSIONS SUMMARY
SLAPOUT BOOSTER STATION
DCP OPERATING COMPANY, LP

Emissions Source	Emission Point Identification	Criteria Pollutants ¹							
		NO _x		VOC		CO		Formaldehyde	
		(lb/hr)	(T/yr)	(lb/hr)	(T/yr)	(lb/hr)	(T/yr)	(lb/hr)	(T/yr)
Superior 8G835 Compressor Engine (667 Hp) ²	ENG-1a	4.85	21.25	3.24	14.17	4.85	21.25	0.02	0.10
Superior 8G835 Compressor Engine (667 Hp) ²	ENG-2a	4.85	21.25	3.24	14.17	4.85	21.25	0.02	0.10
Superior 8G835 Compressor Engine (667 Hp) ²	ENG-3	4.85	21.25	3.24	14.17	4.85	21.25	0.02	0.10
Condensate Storage Tank (300-bbl)	TNK-7	—	—	—	3.38	—	--	—	—
Methanol Storage Tank (210-bbl)	TNK-8	—	—	—	0.56	—	--	—	—
Methanol Storage Tank (25-bbl)	TNK-2	—	—	—	0.08	—	--	—	—
Methanol Storage Tank (25-bbl)	TNK-3	—	—	—	0.08	—	--	—	—
Condensate Truck Loading	LOAD-1	—	—	—	1.50	—	--	—	—
Blowdown Emissions	BD-1	—	—	—	3.73	—	--	—	—
Maintenance, Startups, and Shutdowns	MSS-1	—	—	25.85	1.01	—	--	—	—
Process Piping Fugitive Emissions	FUG-1	—	—	—	7.74	—	--	—	—
Facility Emissions		14.56	63.76	35.56	60.58	14.56	63.76	0.07	0.30

Notes:

1. Emissions of SO₂ and PM are assumed to be negligible and not reportable.
2. Refer to Attachment 4 for compressor engines emission calculations.

ATTACHMENT 4

Engine Potential Emissions Calculations

**POTENTIAL EMISSIONS SUMMARY
DCP OPERATING COMPANY, LP
SUPERIOR 8G825 (ENG-1a)
SLAPOUT BOOSTER STATION**

Pollutant ¹	Horsepower	Emission Factors ²	Potential Emission Rate ³		Safety Factor (%)	Proposed Emission Rate	
		(grams/Hp-hr)	(lb/hr)	(T/yr)		(lb/hr)	(T/yr)
NO _x	667	3.00	4.41	19.32	10%	4.85	21.25
VOC	667	2.00	2.94	12.88	10%	3.24	14.17
CO	667	3.00	4.41	19.32	10%	4.85	21.25
FORMALDEHYDE	667	0.01	0.01	0.03	200%	0.02	0.10

Notes:

1. Emissions of SO₂ and PM are assumed to be negligible and not reportable.
2. Emission factors obtained from manufacturer data.
3. Potential emissions based on emission factors, maximum horsepower, a brake specific fuel consumption of 8,000 btu/hp-hr, operation of a catalytic converter, and 8,760 hours of operation per year.

**SUPERIOR 8G825 (ENG-2a)
SLAPOUT BOOSTER STATION**

Pollutant ¹	Horsepower	Emission Factors ²	Potential Emission Rate ³		Safety Factor (%)	Proposed Emission Rate	
		(grams/Hp-hr)	(lb/hr)	(T/yr)		(lb/hr)	(T/yr)
NO _x	667	3.00	4.41	19.32	10%	4.85	21.25
VOC	667	2.00	2.94	12.88	10%	3.24	14.17
CO	667	3.00	4.41	19.32	10%	4.85	21.25
FORMALDEHYDE	667	0.01	0.01	0.03	200%	0.02	0.10

Notes:

1. Emissions of SO₂ and PM are assumed to be negligible and not reportable.
2. Emission factors obtained from manufacturer data.
3. Potential emissions based on emission factors, maximum horsepower, a brake specific fuel consumption of 8,000 btu/hp-hr, operation of a catalytic converter, and 8,760 hours of operation per year.

**SUPERIOR 8G825 (ENG-3)
SLAPOUT BOOSTER STATION**

Pollutant ¹	Horsepower	Emission Factors ²	Potential Emission Rate ³		Safety Factor (%)	Proposed Emission Rate	
		(grams/Hp-hr)	(lb/hr)	(T/yr)		(lb/hr)	(T/yr)
NO _x	667	3.00	4.41	19.32	10%	4.85	21.25
VOC	667	2.00	2.94	12.88	10%	3.24	14.17
CO	667	3.00	4.41	19.32	10%	4.85	21.25
FORMALDEHYDE	667	0.01	0.01	0.03	200%	0.02	0.10

Notes:

1. Emissions of SO₂ and PM are assumed to be negligible and not reportable.
2. Emission factors obtained from manufacturer data.
3. Potential emissions based on emission factors, maximum horsepower, a brake specific fuel consumption of 8,000 btu/hp-hr, operation of a catalytic converter, and 8,760 hours of operation per year.

**SUPERIOR NATURALLY ASPIRATED ENGINES
MODEL 8G-825**

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ENGINE SPECIFICATIONS

Type	Four(4)-Cycle
Aspiration	Naturally Aspirated
Cylinder Configuration	Inline
Number of Cylinders	Eight (8)
Bore - in. (mm)	10 (254)
Stroke - in. (mm)	10.50 (266.7)
Displacement - cu.in. (liter)	6597 (108.15)
Compression Ratio	10 : 1
Power Rated - BHP (kW)	800 (600)
Speed Rated - RPM	900
Piston Speed - FPM(m/s)	1575 (8.0)
Speed Range - RPM	900 - 500
Ignition System	Non-Shielded, Altronic III
Fuel system	Carbureted with Final Cut Regulator
Governor	Hydraulic (UG-8L) With Manual Speed Setting
Exhaust Manifold	Totally Water Cooled
Jacket Water Pump	Built-In Centrifugal, Belt Driven
Jacket Water Thermostat	Engine Mounted
Lube Oil Pump	Gear Type with Pressure Regulating Valve
Lube Oil Thermostat	Engine Mounted
Prelube Pump	Manual, Mounted and Piped
Lube Oil Cooler	Shell & Tube Type, Mounted and Piped
Crankcase Breather	Positive Ventilation
Crankcase Doors	Pressure Relief (Bicera Type) Doors
Direction of Rotation	Counterclockwise From Flywheel End



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**SUPERIOR NATURALLY ASPIRATED ENGINES
MODEL 8G-825**

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PERFORMANCE

Engine Operating Data	See Page 211 & 212	
Rating Conditions		
-Altitude	feet	1500
	meter	(457)
-Temperature	Deg F	90
	Deg C	(32.2)
Rated Torque Over 900-500 RPM Range	lb-ft	4668
	M-kg	(646)
Brake Mean Effective Pressure Rating/BMEP	psi	106.7
	kg/cm2	(7.50)
Rated Brake Specific Fuel Consumption/BSFC (Plus or Minus 3 Percent Factory Tolerance)	Btu/bhp-hr	7750
	kcal/kW-hr	(2619)
Heat Rejection Data	See Page 211 & 212	
Emissions	See Page 213	

STARTING SYSTEM

Air/Gas Starting Motor Make & Model	IR / SS-825	
Number of Starting Motors	One(1)	
Supply Air/Gas Pressure	psi	150
	kg/cm2	(10.5)
Consumption Rate/Starter Motor		
-Air	scfm	1400
	liter/sec	(661)
-Gas	scfm	1663
	liter/sec	(785)
-Normal Starting Time	sec	15
Connection Sizes		
-Inlet	1-1/2 In. NPT	
-Outlet	2-1/2 In. NPT	
-Optional: Inlet Flange	1-1/2 In. Square	
Outlet Flange	2-1/2 In. 150 Lb.	



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**SUPERIOR NATURALLY ASPIRATED ENGINES
MODEL 8G-825**

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AIR INTAKE SYSTEM

Intake Air Flow Rate	See Page 211 & 212
Max. Allowable Pressure Drop	In H ₂ O 7.5 mm H ₂ O (191)
Air Intake, Inlet Connection	Flex Connection for 8 In. Pipe

FUEL SYSTEM

Required Fuel Gas Pressure to Engine Based on Pipeline Quality Natural Gas	psi 5-10 kg/cm ² (0.4-0.7)
Gas Inlet Connection	2 In. NPT

EXHAUST SYSTEM

Max. Allowable Back Pressure	In H ₂ O 15 mm H ₂ O (381)
Exhaust Outlet Flange Connection Size	10 In. 150 Lb. FF
Exhaust Flow Rate	See Page 211 & 212
Stack Temperature	See Page 211 & 212



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**SUPERIOR NATURALLY ASPIRATED ENGINES
MODEL 8G-825**

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COOLING SYSTEM

Jacket Water Capacity - Engine Only	Gallon	62
	liter	(235)
Jacket Water Pump		
-Jacket Water Outlet Temperature, Normal	Deg F	170-180
	Deg C	(76-82)
-Flow Rate at Rated Speed	GPM	275
	liter/sec	(17.3)
-Available External Head:		
Straight Vane(Standard)	psi	21
	kg/cm2	(1.48)
-Minimum NPSH Required:		
Straight Vane(Standard)	feet	18
	meter	(5.49)
Connection Sizes		
-Jacket Water Inlet	4 In. NPT	
-Jacket Water Outlet	3 In. NPT	
-Vent Line to Surge Tank, Minimum Size	3/8 In. Tubing	
-Surge Tank Return to Pump Inlet	1-1/2 In. NPT	

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SUPERIOR NATURALLY ASPIRATED ENGINES
MODEL 8G-825

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LUBRICATION SYSTEM

Lube Oil Sump Capacity	Gallon liter	80 (303)
Lube Oil Consumption(Estimated)	Gal/Day liter/Day	1.60 (6.06)
Lube Oil Pressure - Normal	psi kg/cm2	35-40 (2.5-2.8)
Temperature Into Engine - Normal	Deg F Deg C	160-170 (71-77)
Flow Rate Through Oil Filter	GPM liter/sec	40 (2.52)
Lube Oil Filters, Engine Mounted(Standard)		
-Type	Full Flow	
-Microns of Filtration	Fifteen(15)	
Connection Size		
-Lube Oil Sump Drain Plug	1-1/2 In. NPT	



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**SUPERIOR NATURALLY ASPIRATED ENGINES
MODEL 8G-825**

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BEARING DIMENSIONS

Main Bearing, Split Shell

-Diameter	In	6.00
	mm	(152.4)
-Width	In	3.50
	mm	(88.9)
-Quantity	Nos.	9

Crankpin Bearing, Split Shell

-Diameter	In	5.75
	mm	(146.0)
-Width	In	3.63
	mm	(92.1)
-Quantity	Nos.	8

Wrist Pin Bearing

-Diameter	In	3.50
	mm	(88.9)
-Width	In	3.16
	mm	(80.3)
-Quantity	Nos.	8

Camshaft Bearing, Split Shell

-Diameter	In	2.25
	mm	(57.2)
-Width	In	1.63
	mm	(41.3)
-Quantity	Nos.	10

DIMENSIONS AND WEIGHT (APPROXIMATE)

Overall Length	In	139
	mm	(3531)
Overall Width	In	67
	mm	(1702)
Overall Height	In	75
	mm	(1905)
Dry Weight	Lb	20500
	kg	(9299)



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MODEL 8G-825**

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MISCELLANEOUS

Clearance Required to Remove Piston	In	81.75
	mm	(2076)
Heaviest Engine Parts (Approximate Weights)		
-Cylinder Block Assembly	Lb	4400
	kg	(1996)
-Cylinder Head Assembly	Lb	250
	kg	(113)
-Piston and Connecting Rod Assembly	Lb	192
	kg	(87)
-Exhaust Manifold	Lb	430
	kg	(195)



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**MAXIMUM UNBALANCED FORCES AND COUPLES
DUE TO MANUFACTURING TOLERANCES
(IN ENGLISH UNITS)**

The following data are based on the assumption that engine components may be machined to a maximum and/or minimum permissible weight limitations, and that assembly may be made in such manner that maximum unbalanced forces or couples may be produced. It is to be noted, that an unbalanced assembly which produces a maximum unbalanced force tends to produce a minimum unbalanced couple or vice-versa. It is also to be noted, that these are maximum calculated values; standard assembly procedures will rarely produce such an extreme conditions and normal expectations should not exceed 50 percent of the calculated values.

ENGINE RPM	PRIMARY FORCE - Lb.		SECONDARY FORCE - Lb.	
	VERTICAL	HORIZONTAL	VERTICAL	HORIZONTAL
900	789.428	447.713	120.814	0
800	623.745	353.784	95.458	0
700	477.555	270.839	73.085	0
600	350.857	198.984	53.695	0

ENGINE RPM	PRIMARY COUPLE - Lb.Ft.		SECONDARY COUPLE - Lb.Ft.	
	VERTICAL	HORIZONTAL	VERTICAL	HORIZONTAL
900	1945.844	1160.555	261.763	0
800	1537.457	916.982	206.825	0
700	1177.116	702.064	158.350	0
600	864.820	515.802	116.339	0



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ENGINE OPERATING DATA AND HEAT REJECTION SUPERIOR 8G825						
	PERCENT RATED LOAD	BMEP (PSI)	ENGINE SPEED - RPM			
			900	800	700	600
BRAKE HORSEPOWER (BHP)	110	117	880	782	684	586
	100	107	800	711	622	533
	75	80	600	533	467	400
	50	53	400	356	311	267
BRAKE SPECIFIC FUEL CONSUMPTION (BTU/BHP-HR)	110	117	—	—	—	—
	100	107	7750	7750	7800	7850
	75	80	8510	8550	8500	8500
	50	53	10150	10000	9900	9900
INTAKE AIR FLOW REQUIREMENT (SCFM)	110	117	1261	1150	1009	854
	100	107	1186	1055	927	791
	75	80	945	836	745	635
	50	53	727	636	566	482
EXHAUST FLOW (LB/MIN)	110	117	99	92	81	69
	100	107	96	85	75	64
	75	80	78	67	59	51
	50	53	59	51	46	39
EXHAUST TEMP. (+50°F)	110	117	1330	1320	1305	1270
	100	107	1340	1315	1305	1250
	75	80	1310	1280	1225	1140
	50	53	1220	1190	1160	1110
JACKET WATER HEAT REJECTION (BTU/MIN)	110	117	29550	26550	23730	21360
	100	107	29100	26450	23730	21090
	75	80	28090	25100	22640	20000
	50	53	24090	21360	18636	16360
LUBE OIL HEAT REJECTION (BTU/MIN)	110	117	3600	3600	3600	3600
	100	107	3600	3600	3600	3500
	75	80	3600	3510	3400	3400
	50	53	3420	3240	3240	3200

NOTES :

- 1) FUEL CONSUMPTION BASED ON PIPELINE QUALITY FUEL AND ENGINE ADJUSTMENT FOR STANDARD EXHAUST EMISSION RATES, SUBJECT TO $\pm 3\%$ TOLERANCE FOR FACTORY TESTS.
- 2) HEAT REJECTION DATA ARE BASED ON NOMINAL 180°F JACKET WATER OUTLET TEMPERATURE. REFER TO GENERAL DATA SECTION, PAGE GEN-211/9-88 FOR HEAT REJECTION ADJUSTMENT FACTORS DUE TO HOT WATER SYSTEMS OR EBULLIENT COOLING.
HEAT REJECTION DATA ARE AVERAGE VALUES AND WILL VARY WITH OPERATING CONDITIONS AND AMBIENT TEMPERATURE. ADD RESERVE FACTOR FOR SIZING COOLING SYSTEMS. SUBTRACT 10% RESERVE FACTOR TO COMPUTE RECOVERABLE HEAT.



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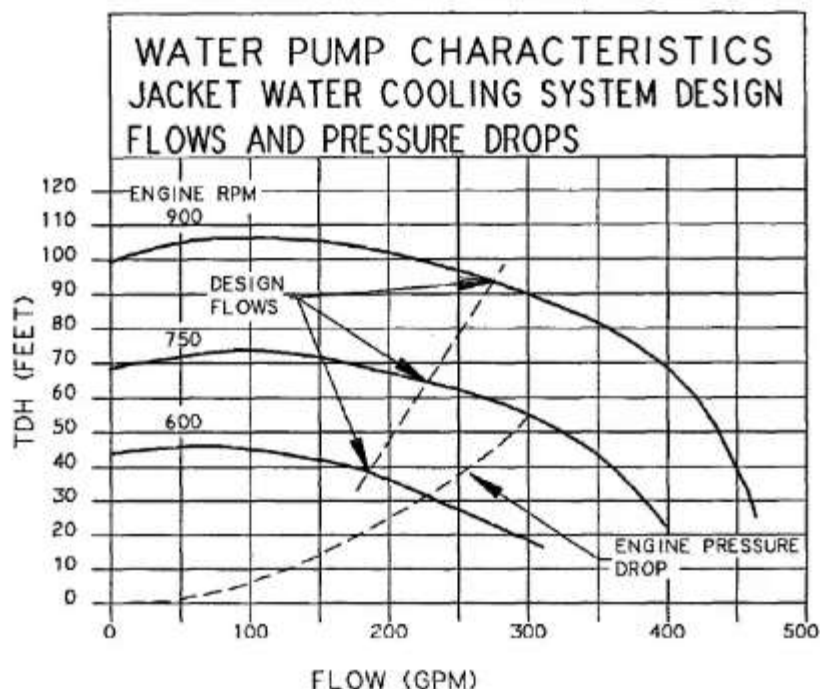
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**SUPERIOR NATURALLY ASPIRATED GAS ENGINE
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IMPELLER P/N C-026-376 (STRAIGHT VANE)
PUMP RPM = 2.167 X ENGINE RPM
DIRECTION OF ROTATION (BI-DIRECTIONAL CAPABILITY)
NORMALLY CW (FACING DRIVE END)
NPSH_R = 18.0 FEET @ 900 RPM & 275 GPM
EXTERNAL HEAD = THE DIFFERENCE BETWEEN THE
SYSTEM PRESSURE DROP AND THE ENGINE PRESSURE DROP
AT THAT FLOWRATE. FOR EXAMPLE:
EXTERNAL HEAD FOR THE 900 RPM DESIGN FLOWRATE
OF 275 GPM = 94.0 FT. - 45.0 FT. = 49.0 FT.
49.0 FT. + 2.31 = 21.0 PSI
ENGINE PRESSURE DROP INCLUDES ALL SUPERIOR SUPPLIED COMPONENTS.



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ATTACHMENT 5

Storage Tank Potential Emissions Calculations

**POTENTIAL EMISSIONS SUMMARY
CONDENSATE STORAGE TANK EMISSIONS
SLAPOUT BOOSTER STATION
DCP OPERATING COMPANY, LP**

Emissions Unit	Source	Annual Throughput (gallons/year)	Tank Capacity (gallons)	Potential VOC Emissions ¹							
				Annual Breathing Losses ² (T/yr)	Annual Working Losses ² (T/yr)	Annual Flash Losses ² (T/yr)	Annual Uncontrolled Emissions (T/yr)	Combustor Capture & Control Efficiency ³ (%)	Controlled Annual Emissions (T/yr)	Safety Factor (%)	Proposed Annual Emissions (T/yr)
TNK-7	Condensate Storage Tank (300-bbl)	150,000	12,600	0.87	0.37	2.13	3.38	0%	3.38	0%	3.38
TNK-8	Methanol Storage Tank (210-bbl)	150,000	8,820	0.111	0.17	0.00	0.28	0%	0.28	100%	0.56
TNK-2	Methanol Storage Tank (25-bbl)	124,993	1,050	0.019	0.021	0.00	0.04	0%	0.04	100%	0.08
TNK-3	Methanol Storage Tank (25-bbl)	124,993	1,050	0.019	0.021	0.00	0.04	0%	0.04	100%	0.08

1. Based on maximum annual condensate throughput value of 150,000-gal/yr.
2. Annual working, and breathing losses were determined using ProMax process simulation software.

Emissions Unit	Source	Annual Throughput (gallons/year)	Tank Capacity (gallons)	Potential Methane Emissions ¹					
				Annual Breathing Losses ² (T/yr)	Annual Working Losses ² (T/yr)	Annual Flash Losses ³ (T/yr)	Annual Uncontrolled Emissions	Combustor Capture & Control Efficiency ³ (%)	Controlled Annual Emissions (T/yr)
TNK-7	Condensate Storage Tank (300-bbl)	150,000	12,600	0.11	0.04	1.09	1.24	0%	1.24
TNK-8	Methanol Storage Tank (210-bbl)	150,000	8,820	0.00	0.00	0.00	0.00	0%	0.00
TNK-2	Methanol Storage Tank (25-bbl)	124,993	1,050	0.00	0.00	0.00	0.00	0%	0.00
TNK-3	Methanol Storage Tank (25-bbl)	124,993	1,050	0.00	0.00	0.00	0.00	0%	0.00

1. Based on maximum annual condensate throughput value of 3,571-bbls/yr.
2. Annual flash, working, and breathing losses were determined using ProMax.

CONDENSATE STORAGE TANK EMISSIONS
SLAPOUT BOOSTER STATION
DCP OPERATING COMPANY, LP

Emission Summary [Total]					
Component Subset	Tank Losses	Flashing Losses	Working Losses	Standing Losses	Loading Losses
	[ton/yr]	[ton/yr]	[ton/yr]	[ton/yr]	[ton/yr]
VOCs	3.377	2.132	0.371	0.874	0.177
HAPs	0.276	0.179	0.029	0.068	0.015
BTEX	0.047	0.031	0.005	0.011	0.002
H2S	0.000	0.000	0.000	0.000	0.000

Capture %
0%
VOC Control %
0%
Propane Control %
0%
VRU Downtime

Emission Summary [Per Tank]					
Component Subset	Tank Losses	Flashing Losses	Working Losses	Standing Losses	Loading Losses
	[ton/yr]	[ton/yr]	[ton/yr]	[ton/yr]	[ton/yr]
VOCs	3.377	2.132	0.371	0.874	0.177
HAPs	0.276	0.179	0.029	0.068	0.015
BTEX	0.047	0.031	0.005	0.011	0.002
H2S	0.000	0.000	0.000	0.000	0.000

Stream Properties						
		Tank Inlet	Flashing Losses	Working Losses	Standing Losses	Loading Losses
Molecular Weight	[lb/lbmol]	112.731	30.597	39.800	39.800	51.432
Net Ideal Gas Heating Value	[BTU/scf]	-	1570.932	2020.105	2020.105	2669.206
Standard Vapor Volumetric Flow	[scf/d]	-	270.504	28.629	67.366	7.978
Specific Gravity		0.740	-	-	-	-
Reid Vapor Pressure	[psi]	8.151	-	-	-	-
API Gravity		61.147	-	-	-	-
Standard Liquid Volumetric Flow	[bbl/d]	9.993	-	-	-	-

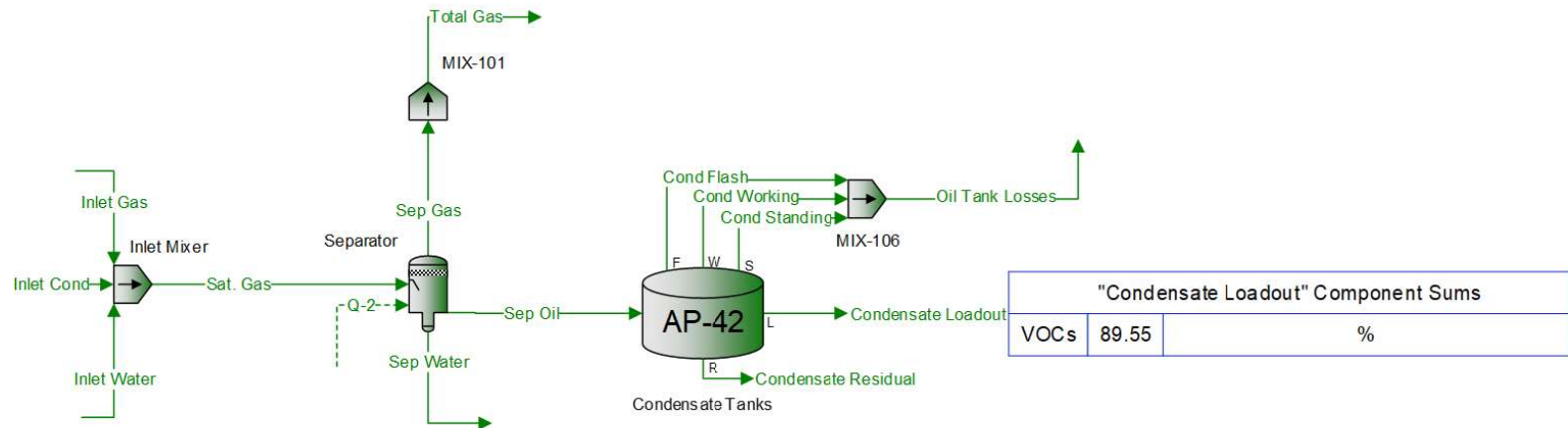
# of Tanks:	1
Vent to Atmosphere	
Uncaptured Emissions at Tank	
Tank Losses	
TPY	
VOC	3.3766
HAPs	0.2759
BTEX	0.047
H2S	0
Methane	1.2386

Emissions after control (0% Destruction)	
Emissions after control at ECD	
Tank Losses	
TPY	
	0
	0
	0
	0
	0

Uncaptured Emissions at Tank	
Tank Losses	
TPY	
VOC	3.3768
HAPs	0.2759
BTEX	0.047
H2S	0
Methane	1.24

Emissions after control at ECD	
Tank Losses	
TPY	
	0
	0
	0
	0
	0.00

Slapout Booster



Names	Units	Inlet Gas	Sep Gas	Oil Tank Losses
Temperature	°F	70	48	68.556
Pressure	psig	5	46	-1.3059
Std Vapor Volumetric Flow	MCFD	0.07025	0.0098401	0.35917
Net Ideal Gas Heating Value	Btu/ft ³	1137.3	1027.8	1688.6
VOC	ton/yr		0.0139	3.309
VOC	lb/h		0.003173	0.7555
Benzene	ton/yr	0.00021	1.4e-05	0.0041
Benzene	lb/h	4.7e-05	3.1e-06	0.00094
H2S	ton/yr	3.178e-06	1.546e-08	2.1816e-06
H2S	lb/h	7.26e-07	3.53e-09	4.98e-07
C3(Mass Flow)	ton/yr	0.062442	0.0067146	1.3498
C3(Mass Flow)	lb/h	0.014256	0.001533	0.30817
C3(Mole Fraction)	%	4.1915	3.2178	17.721
VOC	%		5.4828	34.34

Oil Production: 9.8 bb/d
Oil Production: 150,000 gal/year

VOC (Uncontrolled)

Oil Tank (Total): 3.4 ton/yr

VOC -- Oil Loading Losses: 0.1767 ton/yr

Inlet Stream Summary		
Stream Name		Inlet Cond
Stream Flowsheet		Storage Tanks
Temperature	°F	70.000
Pressure	psig	5.000
Standard Vapor Volumetric Flow	MSCFD	8.500
Standard Liquid Volumetric Flow	bbl/d	9.965
Vapor Fraction	(%)	1.538
Component		[Mol%]
H2S		0.000
N2		0.000
CO2		0.103
C1		1.306
C2		0.896
C3		2.119
iC4		0.721
nC4		2.678
2,2-Dimethylpropane		0.000
Cyclopentane		0.000
iC5		1.850
nC5		3.095
2-Methylpentane		0.000
nC6		7.230
C7		9.050
Methylcyclohexane		1.606
C8		17.566
C9		19.271
C10+		23.122
Cyclohexane		0.000
Benzene		0.139
Toluene		2.234
Ethylbenzene		0.599
m-Xylene		6.415
2,2,4-Trimethylpentane		0.000
Water		0.000

Inlet Stream Summary		
Stream Name		Inlet Gas
Stream Flowsheet		Storage Tanks
Temperature	°F	70.000
Pressure	psig	5.000
Standard Vapor Volumetric Flow	MSCFD	0.070
Standard Liquid Volumetric Flow	bbl/d	0.032
Vapor Fraction	(%)	100.000
Component		[Mol%]
H2S		0.000
N2		0.609
CO2		0.919
C1		82.608
C2		7.017
C3		4.192
iC4		0.606
nC4		1.418
2,2-Dimethylpropane		0.000
Cyclopentane		0.000
iC5		0.392
nC5		0.462
2-Methylpentane		0.333
nC6		0.952
C7		0.272
Methylcyclohexane		0.000
C8		0.136
C9		0.040
C10+		0.004
Cyclohexane		0.000
Benzene		0.008
Toluene		0.017
Ethylbenzene		0.004
m-Xylene		0.009
2,2,4-Trimethylpentane		0.000
Water		0.000

Flowsheet Information				
Tank Losses Block Name		Condensate Tanks		
Tank Losses Block Inlet Stream		Sep Oil		

Tank Characteristics				
Tank Type		Vertical Cylinder		
Time Frame		Year		
Material Category		Light Organics		
Number of Tanks		1		
Shell Height	[ft]	15.000		
Diameter [ft]	[ft]	12.000		
Maximum Liquid Height	[%] [ft]	100.000	15.000	
Average Liquid Height	[%] [ft]	50.000	7.500	
Minimum Liquid Height	[%] [ft]	0.000	0.000	
Sum of Increases in Liquid Level	[ft/yr]	195.889		
Tank Volume	[gal] [bbl]	12690.402	302.152	
Insulation		Uninsulated		
Bolted or Riveted Construction		False		
Vapor Balanced Tank		False		

Paint Characteristics	
Shell Color	Light Grey
Shell Paint Condition	Average
Roof Color	Light Grey
Roof Paint Condition	Average

Roof Characteristics	
Type	Cone
Diameter	[ft]
Slope	[ft/ft]

Breather Vent Settings	
Breather Vacuum Pressure	[psig]
Breather Vent Pressure	[psig]

Loading Loss Parameters	
Cargo Carrier	Tank Truck or Rail Tank Car
Land Based Mode of Operation	Submerged Loading: Dedicated Normal Service
Marine Based Mode of Operation	-
Control Efficiency	[%]
Truck Annual Leak Test Passed	None
Overall Reduction Efficiency	[%]

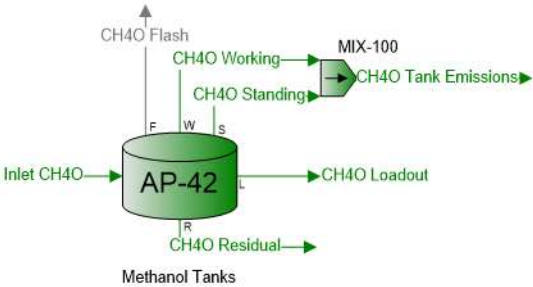
Meteorological Data	
Location	Dodge City, KS
Average Atmospheric Pressure	[psia]
Maximum Average Temperature	[°F]
Minimum Average Temperature	[°F]
Solar Insolation	[BTU/ft^2*day]
Average Wind Speed	[mph]

Tank Conditions	
Flashing Temperature	[°F]
Maximum Liquid Surface Temperature	[°F]
Average Liquid Surface Temperature	[°F]
Known Liquid Bulk Temperature?	False
Bulk Liquid Temperature	[°F]
Net Throughput	[bbl/day] [bbl/yr]
Net Throughput Per Tank	[bbl/day] [bbl/yr]
Annual Turnovers Per Tank	
Residual Liquid	[bbl/day]
Residual Liquid Per Tank	[bbl/day]
Raoult's Law Used for Vapor Pressure Calc?	False
Vapor Pressure @ Minimum Liquid Surface Temperature	[psia]
Vapor Pressure @ Maximum Liquid Surface Temperature	[psia]
Vapor Pressure @ Average Daily Liquid Surface Temperature	[psia]

Tank Conditions	
Heated Tank?	-
Number of Heating Cycles	-
Maximum Liquid Bulk Temperature	[°F]
Minimum Liquid Bulk Temperature	[°F]

Methanol Tank Emissions

Names	Units	Inlet CH4O
Temperature	°F	68.6
Pressure	psia	1.88
Std Liquid Volumetric Flow	bb/day	8.153



"CH4O Tank Emissions" Component Sums		
HAPs	0.03946	ton/yr
VOCs	0.03964	ton/yr

Names	Units	CH4O Working	CH4O Standing	CH4O Tank Emissions
VOC	ton/yr	0.021	0.019	0.04

ATTACHMENT 6

Truck Loading Potential Emissions Calculations

**POTENTIAL EMISSIONS SUMMARY
CONDENSATE TRUCK LOADING (LOAD-1)
SLAPOUT BOOSTER STATION
DCP OPERATING COMPANY, LP**

Material Name	Emissions Unit	Constituent	Saturation Factor ¹ (S)	True Vapor Pressure (P)	Molecular Weight of Vapors (M) (lb/lb-mole)	Temp of Loaded Liquid (F)	Emission Factor ¹ (lb VOC/10 ³ gal)	Annual Throughput ² (gals)	Annual Emissions ³ (T/yr)	Safety Factor (%)	Proposed Emissions (T/yr)
Condensate	LOAD-1	VOC	0.6	3.54	51.43	57.93	2.356	150,000	0.18	750%	1.50

Notes:

1. Loading emissions estimated using ProMax process simulation.
2. Annual Throughput is the amount of condensate loaded out from the tanks.
3. Annual Emissions = Annual Throughput / 1000 x Emission Factor / 2000 lb/T



Bryan Research & Engineering, LLC

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Loading Report		
		Oil
Annual Loading Rate (gal/yr)		149905.550
Saturation Factor		0.600
Temperature (F)		57.931
Temperature (R)		517.601
Pressure (psia)		3.544
Molecular Weight (lb/lbmol)		51.432
VOCs	Loading Loss (lb/hr)	0.040
	Loading Loss (tpy)	0.177
HAPs	Loading Loss (lb/hr)	0.003
	Loading Loss (tpy)	0.015

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<http://www.bre.com/>

Report Navigator can be activated via the ProMax Navigator Toolbar.

ATTACHMENT 7

Blowdown Potential Emissions Calculations

POTENTIAL EMISSIONS FROM BLOWDOWNS (BD-1)
SLAPOUT BOOSTER STATION
DCP OPERATING COMPANY, LP

BLOWDOWN RATES							
Blowdown Rates and Gas Composition							
Volume of Gas (MCF/Hr)		1.5					
Volume of Gas (MCF/Yr)		156					
	Mole %	MCF/Hr	Cu Ft/ #	lbs/hr	MCF/Yr	Cu Ft/ #	lbs/yr
N2	0.61%	0.0092	13.55	0.68	0.95	13.55	70.46
CO2	0.92%	0.0138	8.62	1.61	1.44	8.62	167.04
H2S	0.00%	0.0000	11.14	0.00	0.00	11.14	0.00
C1	82.95%	1.2443	23.65	52.61	129.41	23.65	5,471.74
C2	7.05%	0.1057	12.62	8.37	10.99	12.62	870.98
C3	4.21%	0.0631	8.61	7.33	6.57	8.61	762.61
IC4	0.61%	0.0091	6.53	1.40	0.95	6.53	145.49
NC4	1.42%	0.0214	6.53	3.27	2.22	6.53	340.19
IC5	0.39%	0.0059	5.26	1.12	0.61	5.26	116.85
NC5	0.46%	0.0070	5.26	1.32	0.72	5.26	137.61
C6+	1.37%	0.0205	4.40	4.66	2.13	4.40	484.31
Total	100.00%	1.500		82.38	156.00		8,567.28
Number of Compressors 3 Total VOC per event (lb/hr) 19.11 Total VOC (T/yr) 2.98 Safety Factor 25% Proposed VOC (T/yr) 3.73							

Notes:

1. It is estimated that up to 1500 cubic feet of gas could be vented to the atmosphere during a blowdown event.
2. It is estimated that up to 156 MCF of gas could be released per year from blowdowns from each compressor.

ATTACHMENT 8

MSS Potential Emissions Calculations

POTENTIAL EMISSIONS FROM MSS ACTIVITIES (MSS-1)
SLAPOUT BOOSTER STATION
DCP OPERATING COMPANY, LP

Summary of MSS Activities						
Activity	VOC ¹		PM		Other HAPs	
	(lb/hr)	(T/yr)	(lb/hr)	(T/yr)	(lb/hr)	(T/yr)
Engine, compressor, turbine and other combustion facilities maintenance	0.06	0.25	-	-	-	-
Repair, adjustment, calibration, lubrication and cleaning of site process equipment			-	-	-	-
Replacement of piping components, pneumatic controllers, boiler refractories, wet and dry seals, meters, instruments, analyzers, screens and filters			-	-	-	-
Turbine or engine component swaps			-	-	-	-
Piping used to bypass a facility during maintenance			-	-	-	-
Pigging and purging of piping	0.83	0.02	-	-	-	-
Abrasive blasting, surface preparation and surface coating of facilities and structures used at the site	6.50	0.02	0.68	0.001	0.07	0.0002
Total =	7.39	0.29	0.68	0.001	0.07	0.0002
Safety Factor =	250%	250%	-	-	-	-
Proposed Emissions =	25.85	1.01	-	-	-	-

MSS - Pigging Operations

Description	Pigging
Number of Events per Year	52
Number of Events per hour	1
Volume per Event, scf	50
Stream Specific Gravity	0.6859
Air MW, lb/mole	28.96
Fuel Stream Density, lb/scf	0.0524
VOC Percentage in Gas Stream, wt%	31.64%
VOC Hourly Emission Rate (lb/hr):	0.83
VOC Annual Emission Rate (T/yr):	0.02

MSS - Sandblasting

Description	Sandblasting	
Application Rate ¹	2,000	lb/hr
Operating Hours	4	hr/yr
PM10 Emission Factor ¹	0.00034	lb/lb usage
PM2.5 Emission Factor ¹	0.00005	lb/lb usage
PM10 Emissions	0.68	lb/hr
PM10 Emissions	0.001	T/yr
PM2.5 Emissions	0.10	lb/hr
PM2.5 Emissions	<0.01	T/yr

MSS - Solvent Cleaning

Description	Solvent Cleaning	
Annual Usage	5	gal/yr
Maximum Hourly Usage	1	gal/hr
Density	6.5	lb/gal
VOC Wt%	100%	-
Dipropylene Glycol Methyl Ether Wt%	1%	-
HAP Emissions	0.07	lb/hr
HAP Emissions	0.0002	T/yr
VOC Emissions	6.50	lb/hr
VOC Emissions	0.02	T/yr

Notes:

1. Miscellaneous MSS emissions of 0.25 T/yr are based on TCEQ's Oil and Gas Spreadsheet and is a cap for miscellaneous MSS activities.

ATTACHMENT 9

Process Piping Fugitives Potential Emissions Calculations

**POTENTIAL EMISSIONS SUMMARY
PROCESS PIPING FUGITIVES (FUG-1)
SLAPOUT BOOSTER STATION
DCP OPERATING COMPANY, LP**

Component Type	Type of Service	Number of Components	Oil and Gas Production Emission Factors (lb/hr-component) ¹	Percent VOC ²	Potential VOC Emission Rates ³	
					lb/hr	T/yr
Valves	Gas/Vapor	383	0.00992	23.20%	0.88	3.86
Connectors	Gas/Vapor	1015	0.00086	23.20%	0.20	0.89
Flanges	Gas/Vapor	34	0.00086	23.20%	0.01	0.03
Compressor Seals	Gas/Vapor	4	0.0194	23.20%	0.02	0.08
Relief Valves	Gas/Vapor	21	0.0194	23.20%	0.09	0.41
Valves	Light Liquid	38	0.0055	100.00%	0.21	0.92
Connectors	Light Liquid	3	0.0002	100.00%	0.00	0.00
Totals:	—	1,498	—	—	1.41	6.19
Safety Factor:	—	—	—	—	25%	25%
Proposed Emissions:	—	—	—	—	1.77	7.74

Notes:

1. Emission factors based on EPA's natural gas processing factors for process piping fugitive emissions.
2. Percent VOC for Gas/Vapor service based on a gas analysis from the Facility.
3. Emission rates based on 8,760 hours per year of operation.

**EXTENDED GAS ANALYSIS
SLAPOUT BOOSTER STATION
DCP OPERATING COMPANY, LP**

Component ¹	Molecular Weight	Mol % ²	Molar Weight ³	Average Mass % ⁴
Hydrogen Sulfide	34	0.000%	0.00	0.00%
Oxygen	32	0.000%	0.00	0.00%
Nitrogen	28	0.612%	0.17	0.82%
Carbon Dioxide	44	0.923%	0.41	1.95%
Methane	16	82.953%	13.27	63.85%
Ethane	30	7.046%	2.11	10.17%
Propane	44	4.209%	1.85	8.91%
i-Butane	58	0.609%	0.35	1.70%
n-Butane	58	1.424%	0.83	3.97%
i-Pentane	72	0.394%	0.28	1.36%
n-Pentane	72	0.464%	0.33	1.61%
Hexanes +	86	1.366%	1.17	5.65%
Totals:		100.00%	20.79	100.00%
⁵ VOC Totals:		8.47%	4.82	23.20%

Notes:

1. Typical components listed in gas analysis for field gas.
2. Mol % values obtained from the gas analysis from a representative Facility.
3. Molar weight = Molecular weight x Mol % /100.
4. Average mass % = Molar weight / Total molar weight.
5. VOC Totals include the following components (C3+):
 - Propane
 - i-Butane
 - n-Butane
 - i-Pentane
 - n-Pentane
 - Hexanes +

ATTACHMENT 10

Oil and Gas Representative Sample Information Forms

OIL & GAS REPRESENTATIVE SAMPLE INFORMATION FORM

Please complete this form for each sample used to estimate emissions at the facility and attach to sample lab analysis.

☒	Sample Follows Representative Sampling Guidance Document	OR	☐	Requesting a Case-By-Case Determination*
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* - Please fill out Additional Justification on Page 3.

1	ACTUAL FACILITY INFORMATION				
Company Name		DCP Operating Company, LP			
Facility Name		Slapout Booster Station			
Latitude / Longitude (to 5 decimal places)		Latitude	36.57751	Longitude	-100.05611
List All Current Air Quality Permit Numbers At This Facility		2021-0124-O (M-1)			
Please select the Facility Type:					
☐	Well Site	☒	Natural Gas Compressor Station (Gathering)	☐	Natural Gas Compressor Station (Transmission)
☐		☐		☐	Natural Gas Processing Plant
Permit Action					
☐	Construction*	☐	Modification*	☒	Operation

* - If application is submitted prior to new construction or modification, Box 4 (Facility-Specific Operating Data) and considerations following (Pages 2-3) may be left blank.

2	REPRESENTATIVE FACILITY INFORMATION				
Company Name					
Facility Name					
Latitude / Longitude (to 5 decimal places)		Latitude		Longitude	
List All Current Air Quality Permit Numbers At This Facility					
Please select the Facility Type:					
☐	Well Site	☐	Natural Gas Compressor Station (Gathering)	☐	Natural Gas Compressor Station (Transmission)
☐		☐		☐	Natural Gas Processing Plant

3	SAMPLE INFORMATION				
Sample Being Utilized		☐	Facility-Specific Sample	☒	Representative Facility Sample
Sample is Used to Estimate Emissions for Which Units		TNK-7; TNK-8; TNK-2; TNK-3; LOAD-1			
Sample Date	11/5/2025	Sample Name or Number		Slapout Booster YL05270CX/WC05885	
Sample Point	Inlet Cond	Type of Sample		Spot - Condensate	
Sample Conditions	Pressure (psig)	5	Temperature (°F)	70	
Please Select and Specify the Sampling Method:					
☐	ASTM	☒	GPA	☐	Other
Specify Method: GPA 2145-16 (Properties); 2186-22 (Calculations)					

4	FACILITY-SPECIFIC OPERATING DATA				
Operating Conditions		Pressure (psig)	5	Temperature (°F)	70
API Gravity of Sales Oil		60	Type of Control & Efficiency	None	
Mark the Following That Apply (Based on Calculated Emission Estimates):					
☐	Facility-Wide VOC Emissions > 80 TPY	☐	Facility-Wide VOC Emissions > 200 TPY	☐	Tank and Loading VOC emissions > 50% Total VOC Emissions
☐		☐		☐	*Storage Tanks, w/o control, with VOC Emissions > 4 TPY per Tank
Is Facility-Wide Throughput:					
☒	< 10 bbl/day	☐	< 1,200 bbl/day and controlled by > 95%	☐	> 10 bbl/day and uncontrolled
☐		☐		☐	> 1,200 bbl/day

If requesting a case-by-case determination, the following considerations are not required.

No.	All Sample Considerations	Yes	No
1	Is sample more than three (3) calendar years old?	☐	☒
		☐	☐
If the above answer is yes, a new sample is required or the sample shall be evaluated on a case-by-case basis.			

Only fill out the following tables when using a representative sample.

No.	Calculated Emission Considerations	Yes	No
2a	For true minor and synthetic minor facilities, are VOC emissions more than 80 TPY and then do storage tank and truck loading VOC emissions account for more than 50% of facility-wide VOC emissions?	☐	☐
2b	For major facilities, are VOC emissions more than 200 TPY?	☐	☐
3	Are individual storage tank emissions, not controlled by a combustion device, more than 4 TPY VOC?	☐	☐
4	Are facility-wide emissions of a single HAP greater than 8 TPY or are total HAP emissions greater than 20 TPY? (Excluding HAP emissions from engines)	☐	☐
		☐	☐
If any of the above answers are yes, a facility-specific sample is required.			

No.	Throughput Considerations	Yes	No
5a	Is facility-wide throughput less than 10 bbl/day? ¹	☐	☐
5b	Is facility-wide throughput less than 1,200 bbl/day and controlled by more than 95% with a VRU and/or combustion device? ²	☐	☐
		☐	☐
If either of the above answers are yes, the representative sample does not have to meet the requirements of distance, sampling point and operating parameters.			

Only fill out the following tables for the facility type being represented.

No.	Well Site Considerations	Yes	No
6a	Is Representative Facility less than 10 miles from the Actual Facility and produced in the same formation?	☐	☐
7a	Is the sample point of the Representative Facility within $\pm 20^{\circ}\text{C}$ (36°F) of the Actual Facility?	☐	☐
8a	Is the sample point of the Representative Facility within ± 20 psig of the Actual Facility if greater than 30 psig or is the sample pressure greater than half that of the actual facility if the actual facility operates at less than 30 psig.	☐	☐
9a	Is the sales oil of the Representative Facility within $\pm 5^{\circ}$ API gravity of the Actual Facility?	☐	☐
10a	Was the representative sample taken at or before the last stage of separation of the actual facility, comparatively?	☐	☐
		☐	☐
If any of the above answers are no, a facility-specific sample is required.			

¹ – This applies to Well Sites and Natural Gas Compressor Stations (Gathering and Transmissions);² – This applies to Well Sites and Natural Gas Compressor Station (Gathering).

No.	Natural Gas Compressor Station (Gathering) Considerations	Yes	No
6b	Is Representative Facility less than 10 miles from the Actual Facility?		
7b	Is the sample point of the Representative Facility within $\pm 20^{\circ}\text{C}$ (36°F) of the Actual Facility?		
8b	Is the sample point of the Representative Facility within ± 20 psig of the Actual Facility if greater than 30 psig or is the sample pressure greater than half that of the actual facility if the actual facility operates at less than 30 psig.		
9b	Is the sales oil of the Representative Facility within $\pm 5^{\circ}$ API gravity of the Actual Facility?		
10b	Was the representative sample taken at or before the last stage of separation of the actual facility, comparatively?		
If any of the above answers are no, a facility-specific sample is required. ³			

No.	Natural Gas Compressor Station (Transmission) Considerations	Yes	No
6c	Is Representative Facility upstream from the Actual Facility and on the same pipeline?		
If any of the above answers are no, a facility-specific sample is required.			

No.	Natural Gas Processing Plant Considerations	Yes	No
6d	Is the condensate treated in a condensate stabilizer prior to entering storage tanks or are storage tanks controlled by greater than 95% with a VRU and/or combustion device?		
If any of the above answers are no, a facility-specific sample is required.			

Additional Justification: _____

³ - A representative sample may be use if all the criteria identified above are met except that the representative facility is located at a distance greater than 10 miles from the actual facility, provided a strong written justification is given for the specific instances where no representative facility that meets the above criteria may exist.



LABORATORY REFERENCE NUMBER : **YL05270CX/WC05885**

PHILLIPS 66

ID: **SLAPOUT BOOSTER**
 AREA: **NOT/REC**
 METER: **INLET COND**
 LEASE: **INLET COND**
 OPERATOR: **PHILLIPS 66**
 STATION: **SLAPOUT BOOSTER**
 SAMPLE DATE: **11/5/2025**
 SAMPLE OF: **CONDENSATE**

LINE PRESSURE: **5 PSI**
 LINE TEMPERATURE: **70 F**
 CYLINDER NUMBER: **725 / A-798**
 EFFECTIVE DATE: **NOT/REC**
 SAMPLED BY: **CR**
 ANALYZED BY: **BRENNAN**
 ANALYZED DATE: **11/7/2025**
 SAMPLE TYPE: **SPOT**

For: **PHILLIPS 66**
 Attn: **ACCOUNTS PAYABLE**
 P.O. BOX **982265**
 EL PASO TX **79998**

Physical Properties per GPA 2145-16

Calculations per GPA 2186-22

Note: Zero = Less than detection limit

	<u>MOL%</u>	<u>WEIGHT%</u>	<u>LIQUID VOL. %</u>
NITROGEN	0.000	0.000	0.000
CARBON DIOXIDE	0.105	0.043	0.039
METHANE	1.327	0.199	0.492
ETHANE	0.911	0.256	0.533
PROPANE	2.154	0.887	1.297
ISOBUTANE	0.733	0.398	0.524
N-BUTANE	2.722	1.477	1.875
ISOPENTANE	1.880	1.266	1.502
N-PENTANE	3.145	2.119	2.491
HEXANES	7.489	5.936	6.580
HEPTANES PLUS	79.534	87.419	84.667
	<u>100.000</u>	<u>100.000</u>	<u>100.000</u>

<u>Calculated Value</u>	<u>Total Sample</u>	<u>Heptanes Plus</u>
Molecular Weight	107.103	117.723
Relative Density	0.7415	0.7655
Liquid Density (lbs/gal Absolute Density)	6.182	6.382
Liquid Density (lbs/gal Weight in Air)	6.176	6.376
Cu.Ft./Vapor / Gal. @ 14.696	21.904	20.573
Vapor Pressure (PSIA) @ 100° F	82.930	0.761
API Gravity at 60° F	59.3	53.3
BTU / LB	20188	20065
BTU / GAL.	124796	148414
BTU / Cu. FT. (Vol. IDEAL Gas Fuel @ 14.696)	5697.4	6224.6
Specific Gravity as a Vapor @ 14.696	3.6977	4.0647

Remarks: FT9529
 Remarks:



LABORATORY REFERENCE NUMBER : YL05270CX/WC05885

COMPANY: PHILLIPS 66
AREA / FIELD: NOT/REC
LEASE: INLET COND

SAMPLE DATE: 11/5/2025

	<u>MOL%</u>	<u>WEIGHT%</u>	<u>LIQUID VOL.%</u>
NITROGEN	0.000	0.000	0.000
CARBON DIOXIDE	0.105	0.043	0.039
METHANE	1.327	0.199	0.492
ETHANE	0.911	0.256	0.533
PROPANE	2.154	0.887	1.297
ISOBUTANE	0.733	0.398	0.524
N-BUTANE	2.722	1.477	1.875
ISOPENTANE	1.880	1.266	1.502
N-PENTANE	3.145	2.119	2.491
2,2-Dimethylbutane	1.174	0.945	1.071
2,3-Dimethylbutane & Cyclopentane	1.321	0.972	1.018
2-Methylpentane	1.536	1.236	1.393
3-Methylpentane	1.379	1.110	1.230
n-Hexane	2.079	1.673	1.868
2,2-Dimethylpentane	0.026	0.024	0.026
Methylcyclopentane	1.045	0.821	0.808
2,4-Dimethylpentane	0.007	0.007	0.008
2,2,3- Trimethylbutane	0.000	0.000	0.000
Benzene	0.141	0.103	0.086
3,3-Dimethylpentane	0.042	0.039	0.041
Cyclohexane	2.467	1.939	1.835
2-Methylhexane	1.024	0.958	1.040
2,3-Dimethylpentane	0.284	0.266	0.282
1,1-Dimethylcyclopentane	0.000	0.000	0.000
3-Methylhexane	1.238	1.158	1.242
1,t-3-Dimethylcyclopentane	0.292	0.268	0.264
1,c-3-Dimethylcyclopentane & 3-Ethylpentane	0.312	0.292	0.308
1,t-2-Dimethylcyclopentane & 2,2,4- Trimethylpentane	0.523	0.558	0.594
n-Heptane	4.067	3.805	4.099
Methylcyclohexane	7.681	7.042	6.746
1,1,3- Trimethylcyclopentane & 2,2-Dimethylhexane	0.013	0.014	0.014
2,5-Dimethylhexane & 2,4-Dimethylhexane	0.289	0.308	0.327
Ethylcyclopentane	0.139	0.127	0.122
2,2,3- Trimethylpentane & 1,t-2,c-4- Trimethylcyclopentane	0.288	0.307	0.316
3,3-Dimethylhexane & 1,t-2,c-3- Trimethylcyclopentane	0.199	0.212	0.220
2,3,4- Trimethylpentane & 2,3-Dimethylhexane	0.000	0.000	0.000
Toluene	2.270	1.953	1.661
1,1,2- Trimethylcyclopentane	0.000	0.000	0.000
3,4-Dimethylhexane	0.000	0.000	0.000
2-Methylheptane	2.506	2.673	2.823
4-Methylheptane	0.000	0.000	0.000
1,c-2,t-4- Trimethylcyclopentane	0.000	0.000	0.000
3-Methylheptane & 3,4-Dimethylhexane	1.521	1.622	1.694

LABORATORY REFERENCE NUMBER : **YL05270CX/WC05885**

COMPANY: PHILLIPS 66
AREA / FIELD: NOT/REC
LEASE: INLET COND

SAMPLE DATE: 11/5/2025

	<u>MOL%</u>	<u>WEIGHT%</u>	<u>LIQUID VOL. %</u>
1,c-3-Dimethylcyclohexane & 3-Ethylhexane	2.551	2.673	2.570
1,t-4-Dimethylcyclohexane & 1,c2,t3- Trimethylcyclopentane	0.000	0.000	0.000
2,2,5-Trimethylhexane & 1,1-Dimethylcyclohexane	0.361	0.432	0.450
Methyl-Ethylcyclopentane's & 2,2,4- Trimethylhexane	0.000	0.000	0.000
n-Octane	7.164	7.641	8.018
1,t2 Dimethylcyclohexane & 2,2,4,4- Tetramethylpentane	0.000	0.000	0.000
1,t-3-Dimethylcyclohexane & 1,c-4-Dimethylcyclohexane	0.322	0.337	0.317
Dimethylheptanes & 1 ,c-2,c-3- Trimethylcyclopentane	0.018	0.019	0.018
Isopropylcyclopentane	0.052	0.054	0.051
Dimethylheptanes & Trimethylhexanes	0.117	0.140	0.145
1,c-2-Dimethylcyclohexane	0.789	0.827	0.766
Dimethylheptanes	0.243	0.291	0.298
Ethylcyclohexane	2.468	2.586	2.419
n-Propylcyclopentane	1.020	1.069	1.015
Trimethylcyclohexanes	0.000	0.000	0.000
Ethylbenzene	0.609	0.604	0.514
Dimethylheptanes & Trimethylhexanes	0.668	0.800	0.813
m-Xylene & p-Xylene	5.004	4.960	4.240
2 & 4 Methyloctane & 3,4-Dimethylheptane	0.000	0.000	0.000
Trimethylcyclohexanes	0.000	0.000	0.000
3-Methyloctane	1.327	1.589	1.625
Trimethylcyclohexanes	0.000	0.000	0.000
o-Xylene	1.516	1.503	1.259
Trimethylcyclohexanes & Isobutylcyclopentane	0.000	0.000	0.000
n-Nonane	5.432	6.505	6.678
C9 Naphthenes & C10 Paraffins & Trimethylcyclohexanes	0.000	0.000	0.000
Isopropylbenzene & Trimethylcyclohexanes	0.610	0.685	0.586
C9 Naphthenes & C10 Paraffins	0.423	0.562	0.561
Isopropylcyclohexane	0.727	0.857	0.788
C9 Naphthenes & C10 Paraffins & Cyclooctane	0.000	0.000	0.000
N-Propylcyclohexane	1.764	2.079	1.931
C9 Naphthenes & C10 Paraffins & n-Butylcyclopentane	0.306	0.407	0.408
n-Propylbenzene	0.454	0.509	0.436
C9 Naphthenes & C10 Paraffins & EthylBenzenes	0.000	0.000	0.000
m-Ethyltoluene	1.078	1.210	1.032
p-Ethyltoluene	0.000	0.000	0.000
1,3,5- Trimethylbenzene & 4 & 5 Methylnonane	1.544	1.733	1.478
2-Methylnonane & 3-Ethylloctane	0.000	0.000	0.000
C9 Naphthenes & C10 Paraffins	0.000	0.000	0.000
O-Ethyltoluene & 3-Methylnonane	1.073	1.204	1.008
C9 Naphthenes & C10 Paraffins	0.198	0.263	0.264
tert-Butylbenzene	0.170	0.213	0.181
1,2,4 Trimethylbenzene & Methylcyclooctane	1.168	1.311	1.104
Isobutylcyclohexane & tert- Butylcyclohexane	0.000	0.000	0.000
n-Decane	2.730	3.627	3.661



LABORATORY REFERENCE NUMBER : YL05270CX/WC05885

COMPANY: PHILLIPS 66
AREA / FIELD: NOT/REC
LEASE: INLET COND

SAMPLE DATE: 11/5/2025

	<u>MOL%</u>	<u>WEIGHT%</u>	<u>LIQUID VOL.%</u>
C10 Aromatics & C11 Paraffins	0.501	0.628	0.520
Isobutylbenzene	0.000	0.000	0.000
sec-Butylbenzene	0.000	0.000	0.000
C10 Aromatics & C11 Paraffins	0.195	0.285	0.284
1,2,3-Trimethylbenzene	1.079	1.211	0.999
C10 Aromatics & C11 Paraffins	0.175	0.255	0.254
n-Butylcyclohexane	0.768	1.006	0.929
C10 Aromatics & C11 Paraffins	0.235	0.343	0.342
1,3-Diethylbenzene & 1-Methyl-3-propylbenzene	0.333	0.417	0.356
1,2-Diethylbenzene & n-Butylbenzene	0.412	0.516	0.436
1,4-Diethylbenzene & 1-Methyl-4-propylbenzene	0.402	0.504	0.424
C10 Aromatics & C11 Paraffins	0.869	1.268	1.263
n-Undecane	1.454	2.122	2.114
Dodecane +	4.831	7.678	7.556
	<u>100.000</u>	<u>100.000</u>	<u>100.000</u>

Heavy End Grouping Breakdown

HEXANES	C6	7.489
HEPTANES	C7	11.468
OCTANES	C8	24.982
NONANES	C9	19.585
DECANES	C10	12.245
UNDECANES	C11	6.423
ISODODECANES+	C12+	4.831
Total		87.023 Mol%

BTEX BREAKDOWN

	Mol%	WT.%
BENZENE	0.141	0.103
TOLUENE	2.270	1.953
ETHYLBENZENE	0.609	0.604
XYLENES	6.520	6.463
Total BTEX	9.540	9.123

Calculated Value

Total Sample

Heptanes Plus

Molecular Weight	107.103	117.723
Relative Density	0.7415	0.7655
Liquid Density (lbs/gal Absolute Density)	6.182	6.382
Liquid Density (lbs/gal Weight in Air)	6.176	6.376
Cu.Ft./Vapor / Gal. @ 14.696	21.904	20.573
Vapor Pressure (PSIA) @ 100° F	82.930	0.761
API Gravity at 60° F	59.3	53.3
BTU / LB	20188	20065
BTU / GAL.	124796	148414
BTU / Cu. FT. (Vol. IDEAL Gas Fuel @ 14.696)	5697.4	6224.6
Specific Gravity as a Vapor @ 14.696	3.6977	4.0647



LABORATORY REFERENCE NUMBER : **YL05270CX/WC05885**

PHILLIPS 66

ID: **SLAPOUT BOOSTER**
 AREA: **NOT/REC**
 METER: **INLET COND**
 LEASE: **INLET COND**
 OPERATOR: **PHILLIPS 66**
 STATION: **SLAPOUT BOOSTER**
 SAMPLE DATE: **11/5/2025**
 SAMPLE OF: **CONDENSATE**

LINE PRESSURE: **5 PSI**
 LINE TEMPERATURE: **70 F**
 CYLINDER NUMBER: **725 / A-798**
 EFFECTIVE DATE: **NOT/REC**
 SAMPLED BY: **CR**
 ANALYZED BY: **BRENNAN**
 ANALYZED DATE: **11/7/2025**
 SAMPLE TYPE: **SPOT**

For: **PHILLIPS 66**
 Attn: **ACCOUNTS PAYABLE**
 P.O. BOX **982265**
 EL PASO TX **79998**

Physical Properties per GPA 2145-16

Calculations per GPA 2186-22

Note: Zero = Less than detection limit

	<u>MOL %</u>	<u>WEIGHT%</u>	<u>LIQUID VOL. %</u>
NITROGEN	0.000	0.000	0.000
CARBON DIOXIDE	0.105	0.043	0.039
METHANE	1.327	0.199	0.492
ETHANE	0.911	0.256	0.533
PROPANE	2.154	0.887	1.297
ISOBUTANE	0.733	0.398	0.524
N-BUTANE	2.722	1.477	1.875
ISOPENTANE	1.880	1.266	1.502
N-PENTANE	3.145	2.119	2.491
HEXANE	7.489	5.936	6.580
HEPTANE	11.468	10.238	10.633
OCTANE	24.982	25.004	24.961
NONANE	19.585	21.284	20.158
DECANE	12.245	14.660	13.438
UN-DECANE+	11.254	16.233	15.477
	<u>100.000</u>	<u>100.000</u>	<u>100.000</u>

<u>Calculated Value</u>	<u>Total Sample</u>	<u>Heptanes Plus</u>
Molecular Weight	107.103	117.723
Relative Density	0.7415	0.7655
Liquid Density (lbs/gal Absolute Density)	6.182	6.382
Liquid Density (lbs/gal Weight in Air)	6.176	6.376
Cu.Ft./Vapor / Gal. @ 14.696	21.904	20.573
Vapor Pressure (PSIA) @ 100° F	82.930	0.761
API Gravity at 60° F	59.3	53.3
BTU / LB	20188	20065
BTU / GAL.	124796	148414
BTU / Cu. FT. (Vol. IDEAL Gas Fuel @ 14.696)	5697.4	6224.6
Specific Gravity as a Vapor @ 14.696	3.6977	4.0647

Remarks: FT9529
 Remarks:

OIL & GAS REPRESENTATIVE SAMPLE INFORMATION FORM

Please complete this form for each sample used to estimate emissions at the facility and attach to sample lab analysis.

☒	Sample Follows Representative Sampling Guidance Document	OR	☐	Requesting a Case-By-Case Determination*
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* - Please fill out Additional Justification on Page 3.

1	ACTUAL FACILITY INFORMATION				
Company Name		DCP Operating Company, LP			
Facility Name		Slapout Booster Station			
Latitude / Longitude (to 5 decimal places)		Latitude	36.57751	Longitude	-100.05611
List All Current Air Quality Permit Numbers At This Facility		2021-0124-O (M-1)			
Please select the Facility Type:					
☐	Well Site	☒	Natural Gas Compressor Station (Gathering)	☐	Natural Gas Compressor Station (Transmission)
☐		☐		☐	Natural Gas Processing Plant
Permit Action					
☐	Construction*	☐	Modification*	☒	Operation

* - If application is submitted prior to new construction or modification, Box 4 (Facility-Specific Operating Data) and considerations following (Pages 2-3) may be left blank.

2	REPRESENTATIVE FACILITY INFORMATION				
Company Name					
Facility Name					
Latitude / Longitude (to 5 decimal places)		Latitude		Longitude	
List All Current Air Quality Permit Numbers At This Facility					
Please select the Facility Type:					
☐	Well Site	☐	Natural Gas Compressor Station (Gathering)	☐	Natural Gas Compressor Station (Transmission)
☐		☐		☐	Natural Gas Processing Plant

3	SAMPLE INFORMATION				
Sample Being Utilized		☒	Facility-Specific Sample	☐	Representative Facility Sample
Sample is Used to Estimate Emissions for Which Units		TNK-7; TNK-8; TNK-2; TNK-3; ENG-1a; ENG-2a; ENG-3; LOAD-1; BD-1; MSS-1; FUG-1			
Sample Date		11/5/2025	Sample Name or Number		Slapout Booster LG22106GX/N95153
Sample Point		Gas	Type of Sample		Spot
Sample Conditions		Pressure (psig)	5	Temperature (°F)	70
Please Select and Specify the Sampling Method:					
☐	ASTM	☒	GPA	☐	Other
Specify Method: 2145-16 (Properties); 2286-24 (Calculations)					

4	FACILITY-SPECIFIC OPERATING DATA				
Operating Conditions		Pressure (psig)	5	Temperature (°F)	70
API Gravity of Sales Oil		60	Type of Control & Efficiency		None
Mark the Following That Apply (Based on Calculated Emission Estimates):					
☐	Facility-Wide VOC Emissions > 80 TPY	☐	Facility-Wide VOC Emissions > 200 TPY	☐	Tank and Loading VOC emissions > 50% Total VOC Emissions
☐		☐		☐	*Storage Tanks, w/o control, with VOC Emissions > 4 TPY per Tank
Is Facility-Wide Throughput:					
☒	< 10 bbl/day	☐	< 1,200 bbl/day and controlled by > 95%	☐	> 10 bbl/day and uncontrolled
☐		☐		☐	> 1,200 bbl/day

If requesting a case-by-case determination, the following considerations are not required.

No.	All Sample Considerations	Yes	No
1	Is sample more than three (3) calendar years old?	☐	☒
If the above answer is yes, a new sample is required or the sample shall be evaluated on a case-by-case basis.			

Only fill out the following tables when using a representative sample.

No.	Calculated Emission Considerations	Yes	No
2a	For true minor and synthetic minor facilities, are VOC emissions more than 80 TPY and then do storage tank and truck loading VOC emissions account for more than 50% of facility-wide VOC emissions?	☐	☐
2b	For major facilities, are VOC emissions more than 200 TPY?	☐	☐
3	Are individual storage tank emissions, not controlled by a combustion device, more than 4 TPY VOC?	☐	☐
4	Are facility-wide emissions of a single HAP greater than 8 TPY or are total HAP emissions greater than 20 TPY? (Excluding HAP emissions from engines)	☐	☐
If any of the above answers are yes, a facility-specific sample is required.			

No.	Throughput Considerations	Yes	No
5a	Is facility-wide throughput less than 10 bbl/day? ¹	☐	☐
5b	Is facility-wide throughput less than 1,200 bbl/day and controlled by more than 95% with a VRU and/or combustion device? ²	☐	☐
If either of the above answers are yes, the representative sample does not have to meet the requirements of distance, sampling point and operating parameters.			

Only fill out the following tables for the facility type being represented.

No.	Well Site Considerations	Yes	No
6a	Is Representative Facility less than 10 miles from the Actual Facility and produced in the same formation?	☐	☐
7a	Is the sample point of the Representative Facility within $\pm 20^{\circ}\text{C}$ (36°F) of the Actual Facility?	☐	☐
8a	Is the sample point of the Representative Facility within ± 20 psig of the Actual Facility if greater than 30 psig or is the sample pressure greater than half that of the actual facility if the actual facility operates at less than 30 psig.	☐	☐
9a	Is the sales oil of the Representative Facility within $\pm 5^{\circ}$ API gravity of the Actual Facility?	☐	☐
10a	Was the representative sample taken at or before the last stage of separation of the actual facility, comparatively?	☐	☐
If any of the above answers are no, a facility-specific sample is required.			

¹ – This applies to Well Sites and Natural Gas Compressor Stations (Gathering and Transmissions);² – This applies to Well Sites and Natural Gas Compressor Station (Gathering).

No.	Natural Gas Compressor Station (Gathering) Considerations	Yes	No
6b	Is Representative Facility less than 10 miles from the Actual Facility?		
7b	Is the sample point of the Representative Facility within $\pm 20^{\circ}\text{C}$ (36°F) of the Actual Facility?		
8b	Is the sample point of the Representative Facility within ± 20 psig of the Actual Facility if greater than 30 psig or is the sample pressure greater than half that of the actual facility if the actual facility operates at less than 30 psig.		
9b	Is the sales oil of the Representative Facility within $\pm 5^{\circ}$ API gravity of the Actual Facility?		
10b	Was the representative sample taken at or before the last stage of separation of the actual facility, comparatively?		
If any of the above answers are no, a facility-specific sample is required. ³			

No.	Natural Gas Compressor Station (Transmission) Considerations	Yes	No
6c	Is Representative Facility upstream from the Actual Facility and on the same pipeline?		
If any of the above answers are no, a facility-specific sample is required.			

No.	Natural Gas Processing Plant Considerations	Yes	No
6d	Is the condensate treated in a condensate stabilizer prior to entering storage tanks or are storage tanks controlled by greater than 95% with a VRU and/or combustion device?		
If any of the above answers are no, a facility-specific sample is required.			

Additional Justification: _____

³ - A representative sample may be use if all the criteria identified above are met except that the representative facility is located at a distance greater than 10 miles from the actual facility, provided a strong written justification is given for the specific instances where no representative facility that meets the above criteria may exist.



LABORATORY REFERENCE NUMBER : **LG22106GX/N95153**

PHILLIPS 66

ID: **SLAPOUT BOOSTER**
 AREA: **NOT/REC**
 METER: **INLET GAS**
 LEASE: **INLET GAS**
 OPERATOR: **PHILLIPS 66**
 STATION: **SLAPOUT BOOSTER**
 SAMPLE DATE: **11/5/2025**
 SAMPLE OF: **GAS**

LINE PRESSURE: **VAC PUMP**
 LINE TEMPERATURE: **70 F**
 CYLINDER NUMBER: **4693 / 5300**
 EFFECTIVE DATE: **NOT/REC**
 SAMPLED BY: **CR**
 ANALYZED BY: **BRENNAN**
 ANALYZED DATE: **11/7/2025**
 SAMPLE TYPE: **SPOT**

For: **PHILLIPS 66**
 Attn: **ACCOUNTS PAYABLE**
 P.O. BOX **982265**
 EL PASO TX **79998**

Physical Properties per GPA 2145-16

Calculations per GPA 2286-24

Note: Zero = Less than detection limit

	<u>MOL%</u>	<u>WEIGHT%</u>	<u>GPM @ 14.73</u>
NITROGEN	0.612	0.818	0.068
CARBON DIOXIDE	0.923	1.939	0.158
METHANE	82.953	63.511	14.109
ETHANE	7.046	10.111	1.891
PROPANE	4.209	8.858	1.163
ISOBUTANE	0.609	1.689	0.200
N-BUTANE	1.424	3.950	0.450
ISOPENTANE	0.394	1.357	0.145
N-PENTANE	0.464	1.598	0.169
HEXANES PLUS	1.366	6.169	0.571
	100.000	100.000	18.924

BTU	Vol. Ideal	Vol. Real
	Gas Fuel	Gas Fuel
BTU @ 14.73 PSIA (DRY)	1241.5	1245.9
BTU @ 14.73 PSIA (SAT.)	1219.9	1224.7
Specific Gravity	0.7235	0.7257
Compressibility (Z)	0.9965	

Gasoline Content (Gallons Per Thousand - GPM)

Ethane & Heavier	4.589
Propane & Heavier	2.698
Butane & Heavier	1.535
Pentane & Heavier	0.885
Total 26 psi Reid V.P. Gasoline GPM	1.415

Remarks: FT9529

Remarks:

LABORATORY REFERENCE NUMBER : **LG22106GX/N95153**

COMPANY: PHILLIPS 66
AREA / FIELD: NOT/REC
LEASE: INLET GAS

SAMPLE DATE: 11/5/2025

	<u>MOL%</u>	<u>WEIGHT%</u>	<u>GPM @ 14.73</u>
NITROGEN	0.612	0.818	0.068
CARBON DIOXIDE	0.923	1.939	0.158
METHANE	82.953	63.511	14.109
ETHANE	7.046	10.111	1.891
PROPANE	4.209	8.858	1.163
ISOBUTANE	0.609	1.689	0.200
N-BUTANE	1.424	3.950	0.450
ISOPENTANE	0.394	1.357	0.145
N-PENTANE	0.464	1.598	0.169
2,2-Dimethylbutane	0.009	0.037	0.004
2,3-Dimethylbutane & Cyclopentane	0.034	0.128	0.012
2-Methylpentane	0.111	0.457	0.046
3-Methylpentane	0.060	0.247	0.025
n-Hexane	0.199	0.818	0.082
2,2-Dimethylpentane	0.003	0.014	0.001
Methylcyclopentane	0.091	0.365	0.032
2,4-Dimethylpentane	0.000	0.000	0.000
2,2,3- Trimethylbutane	0.001	0.005	0.000
Benzene	0.013	0.048	0.004
3,3-Dimethylpentane	0.002	0.010	0.001
Cyclohexane	0.167	0.671	0.057
2-Methylhexane	0.038	0.182	0.018
2,3-Dimethylpentane	0.010	0.048	0.005
1,1-Dimethylcyclopentane	0.000	0.000	0.000
3-Methylhexane	0.046	0.220	0.021
1,t-3-Dimethylcyclopentane	0.015	0.070	0.006
1,c-3-Dimethylcyclopentane & 3-Ethylpentane	0.011	0.053	0.005
1,t-2-Dimethylcyclopentane & 2,2,4- Trimethylpentane	0.016	0.087	0.008
n-Heptane	0.102	0.488	0.047
Methylcyclohexane	0.178	0.834	0.072
1,1,3- Trimethylcyclopentane & 2,2-Dimethylhexane	0.003	0.016	0.001
2,5-Dimethylhexane & 2,4-Dimethylhexane	0.003	0.016	0.002
Ethylcyclopentane	0.006	0.028	0.002
2,2,3- Trimethylpentane & 1,t-2,c-4- Trimethylcyclopentane	0.005	0.027	0.003
3,3-Dimethylhexane & 1,t-2,c-3- Trimethylcyclopentane	0.003	0.016	0.002
2,3,4- Trimethylpentane & 2,3-Dimethylhexane	0.000	0.000	0.000
Toluene	0.035	0.154	0.012
1,1,2- Trimethylcyclopentane	0.002	0.011	0.001
3,4-Dimethylhexane	0.000	0.000	0.000
2-Methylheptane	0.015	0.082	0.008
4-Methylheptane	0.009	0.049	0.005
1,c-2,t-4- Trimethylcyclopentane	0.001	0.005	0.000
3-Methylheptane & 3,4-Dimethylhexane	0.013	0.071	0.007

LABORATORY REFERENCE NUMBER : **LG22106GX/N95153**

COMPANY: PHILLIPS 66
AREA / FIELD: NOT/REC
LEASE: INLET GAS

SAMPLE DATE: 11/5/2025

	<u>MOL%</u>	<u>WEIGHT%</u>	<u>GPM @ 14.73</u>
1,c-3-Dimethylcyclohexane & 3-Ethylhexane	0.015	0.080	0.007
1,t-4-Dimethylcyclohexane & 1,c2,t3- Trimethylcyclopentane	0.010	0.054	0.005
2,2,5-Trimethylhexane & 1,1-Dimethylcyclohexane	0.000	0.000	0.000
Methyl-Ethylcyclopentane's & 2,2,4- Trimethylhexane	0.005	0.031	0.003
n-Octane	0.033	0.180	0.017
1,t2 Dimethylcyclohexane & 2,2,4,4- Tetramethylpentane	0.008	0.043	0.004
1,t-3-Dimethylcyclohexane & 1,c-4-Dimethylcyclohexane	0.004	0.021	0.002
Dimethylheptanes & 1 ,c-2,c-3- Trimethylcyclopentane	0.000	0.000	0.000
Isopropylcyclopentane	0.001	0.005	0.000
Dimethylheptanes & Trimethylhexanes	0.001	0.006	0.001
1,c-2-Dimethylcyclohexane	0.004	0.021	0.002
Dimethylheptanes	0.002	0.012	0.001
Ethylcyclohexane	0.013	0.070	0.006
n-Propylcyclopentane	0.003	0.016	0.001
Trimethylcyclohexanes	0.001	0.006	0.001
Ethylbenzene	0.004	0.020	0.002
Dimethylheptanes & Trimethylhexanes	0.003	0.018	0.002
m-Xylene & p-Xylene	0.020	0.101	0.008
2 & 4 Methyloctane & 3,4-Dimethylheptane	0.000	0.000	0.000
Trimethylcyclohexanes	0.000	0.000	0.000
3-Methyloctane	0.003	0.018	0.002
Trimethylcyclohexanes	0.002	0.012	0.001
o-Xylene	0.004	0.020	0.002
Trimethylcyclohexanes & Isobutylcyclopentane	0.003	0.018	0.002
n-Nonane	0.009	0.055	0.005
C9 Naphthenes & C10 Paraffins & Trimethylcyclohexanes	0.000	0.000	0.000
Isopropylbenzene & Trimethylcyclohexanes	0.002	0.011	0.001
C9 Naphthenes & C10 Paraffins	0.001	0.007	0.001
Isopropylcyclohexane	0.001	0.006	0.000
C9 Naphthenes & C10 Paraffins & Cyclooctane	0.001	0.005	0.000
N-Propylcyclohexane	0.002	0.012	0.001
C9 Naphthenes & C10 Paraffins & n-Butylcyclopentane	0.001	0.007	0.001
n-Propylbenzene	0.000	0.000	0.000
C9 Naphthenes & C10 Paraffins & EthylBenzenes	0.001	0.007	0.001
m-Ethyltoluene	0.000	0.000	0.000
p-Ethyltoluene	0.002	0.011	0.001
1,3,5- Trimethylbenzene & 4 & 5 Methylnonane	0.001	0.006	0.000
2-Methylnonane & 3-Ethyloctane	0.001	0.007	0.001
C9 Naphthenes & C10 Paraffins	0.000	0.000	0.000
O-Ethyltoluene & 3-Methylnonane	0.001	0.006	0.000
C9 Naphthenes & C10 Paraffins	0.000	0.000	0.000
tert-Butylbenzene	0.000	0.000	0.000
1,2,4 Trimethylbenzene & Methylcyclooctane	0.001	0.006	0.000
Isobutylcyclohexane & tert- Butylcyclohexane	0.000	0.000	0.000
n-Decane	0.002	0.014	0.001

LABORATORY REFERENCE NUMBER : **LG22106GX/N95153**

COMPANY: PHILLIPS 66
AREA / FIELD: NOT/REC
LEASE: INLET GAS

SAMPLE DATE: 11/5/2025

	<u>MOL%</u>	<u>WEIGHT%</u>	<u>GPM @ 14.73</u>
C10 Aromatics & C11 Paraffins	0.000	0.000	0.000
Isobutylbenzene	0.000	0.000	0.000
sec-Butylbenzene	0.000	0.000	0.000
C10 Aromatics & C11 Paraffins	0.000	0.000	0.000
1,2,3-Trimethylbenzene	0.000	0.000	0.000
C10 Aromatics & C11 Paraffins	0.000	0.000	0.000
n-Butylcyclohexane	0.000	0.000	0.000
C10 Aromatics & C11 Paraffins	0.000	0.000	0.000
1,3-Diethylbenzene & 1-Methyl-3-propylbenzene	0.000	0.000	0.000
1,2-Diethylbenzene & n-Butylbenzene	0.000	0.000	0.000
1,4-Diethylbenzene & 1-Methyl-4-propylbenzene	0.000	0.000	0.000
C10 Aromatics & C11 Paraffins	0.000	0.000	0.000
n-Undecane	0.000	0.000	0.000
Dodecane +	0.000	0.000	0.000
	<u>100.000</u>	<u>100.000</u>	<u>18.924</u>

Calculated Value**Total Sample****Hexanes Plus**

Molecular Weight	20.954	94.658
Relative Density	0.3522	0.7246
Liquid Density (lbs/gal Absolute Density)	2.936	6.041
Liquid Density (lbs/gal Weight in Air)	2.933	6.035
Cu.Ft./Vapor / Gal. @ 14.73	53.049	24.162
Vapor Pressure @ 100° F	4255.280	3.229
API Gravity at 60° F	270.3	63.8
BTU / LB	22432	20415
BTU / GAL.	65847	123337
BTU / Cu. FT. (Vol. IDEAL Gas Fuel @ 14.696)	1238.6	5091.3
Specific Gravity as a Vapor @ 14.73	0.7218	3.2602

Heavy End Grouping Breakdown

HEXANES	C6	0.413
HEPTANES	C7	0.515
OCTANES	C8	0.336
NONANES	C9	0.085
DECANES	C10	0.017
UNDECANES	C11	0.000
ISODODECANES+	C12+	0.000
Total		1.366 Mol%

BTEX BREAKDOWN

	Mol%	WT.%
BENZENE	0.013	0.048
TOLUENE	0.035	0.154
ETHYLBENZENE	0.004	0.020
XYLENES	0.024	0.121
Total BTEX	0.076	0.343



LABORATORY REFERENCE NUMBER : **LG22106GX/N95153**

PHILLIPS 66

ID: **SLAPOUT BOOSTER**
 AREA: **NOT/REC**
 METER: **INLET GAS**
 LEASE: **INLET GAS**
 OPERATOR: **PHILLIPS 66**
 STATION: **SLAPOUT BOOSTER**
 SAMPLE DATE: **11/5/2025**
 SAMPLE OF: **GAS**

LINE PRESSURE: **VAC PUMP**
 LINE TEMPERATURE: **70 F**
 CYLINDER NUMBER: **4693 / 5300**
 EFFECTIVE DATE: **NOT/REC**
 SAMPLED BY: **CR**
 ANALYZED BY: **BRENNAN**
 ANALYZED DATE: **11/7/2025**
 SAMPLE TYPE: **SPOT**

For: **PHILLIPS 66**
 Attn: **ACCOUNTS PAYABLE**
 P.O. BOX **982265**
 EL PASO TX **79998**

Physical Properties per GPA 2145-16

Calculations per GPA 2286-24

Note: Zero = Less than detection limit

	<u>MOL%</u>	<u>WEIGHT%</u>	<u>GPM @ 14.73</u>
NITROGEN	0.612	0.818	0.068
CARBON DIOXIDE	0.923	1.939	0.158
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PROPANE	4.209	8.858	1.163
ISOBUTANE	0.609	1.689	0.200
N-BUTANE	1.424	3.950	0.450
ISOPENTANE	0.394	1.357	0.145
N-PENTANE	0.464	1.598	0.169
HEXANE	0.413	1.687	0.169
HEPTANE	0.515	2.261	0.205
OCTANE	0.336	1.654	0.147
NONANE	0.085	0.462	0.042
DECANE	0.017	0.105	0.008
UN-DECANE+	0.000	0.000	0.000
	<u>100.000</u>	<u>100.000</u>	<u>18.924</u>

BTU

	Vol. Ideal Gas Fuel	Vol. Real Gas Fuel
BTU @ 14.73 PSIA (DRY)	1241.5	1245.9
BTU @ 14.73 PSIA (SAT.)	1219.9	1224.7
Specific Gravity	0.7235	0.7257
Compressibility (Z)	0.9965	

Gasoline Content (Gallons Per Thousand - GPM)

Ethane & Heavier	4.589
Propane & Heavier	2.698
Butane & Heavier	1.535
Pentane & Heavier	0.885
Total 26 psi Reid V.P. Gasoline GPM	1.415

Remarks: FT9529

Remarks:

Your Receipt

(COPY)

PURCHASE RECEIPT

**Oklahoma Department of Environmental Quality
DEQ OKC**

707 N Robinson
Oklahoma City OK 73102
(405)702-1130
OTC Local Ref ID: 149052314
6/9/2026 11:04 AM

Thank you for your payment to the Department of Environmental Quality.

Status:	APPROVED
Customer Name:	JAY LAUGHIN
Type:	MasterCard
Credit Card Number:	**** * 0271

Items	Location	Quantity	TPE Order ID	Total Amount
Invoice	DEQ OKC	1	137737606	\$750.00
Invoice Number: AQD SLAPOUT BOOSTER STATION				
Additional Information: DCP OPERATING COMPANY LP				
Sub-Activity: 59342				
Invoice	DEQ OKC	1	137737606	\$750.00
Invoice Number: AQD BEAVER BOOSTER STATION				
Additional Information: DCP OPERATING COMPANY LP				
Sub-Activity: 59342				
Total remitted to the Oklahoma Department of Environmental Quality				\$1,500.00
Service Fee	DEQ OKC	1	137738140	\$35.80
Total amount charged				\$1,535.80

From: [Laughlin, Jay](#)
To: [DEQ AQD APU](#)
Subject: [EXTERNAL] DCP - Slapout Booster Station - Standard Operating Permit Application
Date: Tuesday, June 9, 2026 3:31:33 PM
Attachments: [image001.png](#)
[image002.png](#)
[2026_06_09_Slapout_Air_Permit_App_Std_O_\(Signed1\).pdf](#)

Hello. Hope things are well.

Attached please find an application for the Slapout Booster Station. DCP is submitting an individual minor source operating permit application for the Facility and requests that Permit No. 2021-0124-O (M-1) be canceled upon the issuance of the individual operating permit. No new emission sources are being added with this application from those currently authorized by the GP-OGF, which includes Permit No. 2021-0124-O (M-1) and Notices of Modifications that have been submitted for engine changes. Emission estimates for maintenance, startups and shutdown (MSS) activities are represented, which were not required for prior permit applications. Emission estimates have been updated for the compressor blowdowns and fugitives based on a new site-specific gas sample.

If you have any questions, please let me know.

Thanks, Jay



Jay Laughlin, P.E.
Environmental
Oklahoma/Kansas/Michigan/Texas Assets

O: 405-605-3835 | M: 405-543-7892 | E: jay.laughlin@p66.com
715 NE 122nd BLD #3, Suite 150 | Oklahoma City, OK 73114-8194
phillips66.com

